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A Numerical Approach to Assessing Thermally Interacting Multiple Boreholes with Variable Heating Strength

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Abstract: The temperature response in the soil surrounding multiple boreholes is evaluated numerically. The assumption of constant heat flux along the borehole wall is examined by coupling the problem to the heat transfer problem inside the borehole and presenting a model with variable heat flux along the borehole length. A numerical finite volume method in a three dimensional meshed domain is used to model the conduction of heat in the soil surrounding the boreholes. In order to determine the heat flux boundary condition, the analytical quasi-three-dimensional solution to the heat transfer problem of the U-tube configuration inside the borehole [1] is used. This solution takes into account the variation in heating strength along the borehole length due to the temperature variation of the fluid running in the U-tube. Thus, critical depths at which thermal interaction occurs can be determined.

Keywords: geothermal energy; vertical ground heat exchangers; numerical analysis; variable heat flux.

1. Introduction

The use of geothermal energy systems is widespread, having had a revival in the 1980's and recently, but both the sustainability and impact of these systems on the environment are now being

questioned. Due to its efficiency, the use of geothermal energy is advantageous in many cases. However, little research is available to guide regulatory agencies and industry towards designs and installations that maximize their sustainability. One potential hindrance to the sustainability of these systems at their design efficiency is the thermal loss from the system itself, which can affect adjacent systems and the surrounding ground. Studies show that interference effects are present in some installed geothermal systems. The influence of these systems on each other implies that they have a spacing that is smaller than the threshold spacing for such systems to avoid thermal interactions, and indicates that there is a limit to the density of geothermal development that can occur in a given region of the ground.

Many studies in the area of geothermal energy have focused on modeling single ground boreholes, most of which are based on analytical [2-16] and/or numerical methods [17-27]. The models vary in the way heat conduction in the soil is solved and heat transfer outside of the boreholes is coupled to the heat transfer inside of the borehole, and in the way the methods are accelerated. Lee and Lam [24] simulate the performance of borehole heat exchangers (BHEs) using a three-dimensional finite-difference method in rectangular coordinates. Each borehole is approximated by a square column to avoid using fine grids inside the borehole. The authors evaluate the heat transfer inside the borehole based on quasi-steady state conditions, allowing variable temperature and loading along the borehole. Li and Zheng [25] propose a three-dimensional unstructured finite-volume numerical model of a vertical U-tube ground heat exchanger (GHE). They divide the soil into several layers in the axial direction so as to account for axial changes in temperature. To address the effect of the thermal mass of the circulating fluid and the dynamics of fluid transport through the loop, He et al. [26] developed a three-dimensional numerical model that simulates fluid transport in a pipe loop and heat transfer with the ground.

The key limitation in most of the previous studies is the assumption of constant and uniform strength of the heat input from the borehole into the ground, either when the borehole is assumed as a cylinder or when it is further simplified to a line source of heat. Duan et al. [28] and Duan and Naterer [29] study the transient heat conduction from a buried power transmission line tower. In their study they formulated the problem of ground heat transfer with a line source of heat with varying heating strength along its length. However, the physical nature of their problem involved pure conduction along a buried rod in the ground which makes it somewhat different from borehole analysis. Furthermore, the potential existence of thermal interaction among multiple boreholes is identified in the literature, but not formulated, and the affecting parameters have not been assessed in detail. This is another key limitation in the past studies in the area of ground heat exchangers. In order to model interacting borehole systems, Koohi-Fayegh and Rosen [30] evaluate the temperature response in the soil surrounding multiple boreholes in a numerical study. They assumed that the heat flux from the borehole wall is constant and, therefore, that heat conduction in the direction of the borehole length is negligible for a major part of the solution domain.

The current study addresses the shortcomings of the past studies by considering a variable heat flux along walls of multiple boreholes by coupling the problem to the heat transfer problem inside the boreholes. A numerical finite volume method in a three dimensional meshed domain is used to model the conduction of heat in the soil surrounding boreholes. In order to determine the heat flux boundary condition, the analytical quasi-three-dimensional solution to the heat transfer problem of the U-tube configuration inside the borehole [1] is used. This solution takes into account the variation in heating

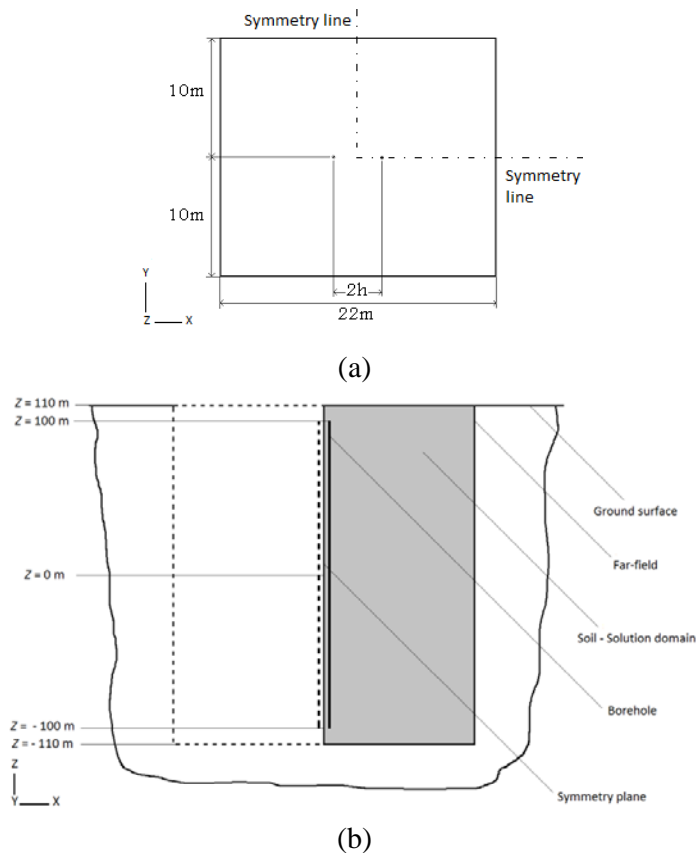
strength along the borehole length due to the temperature variation of the fluid running in the U-tube. Thus, critical depths at which thermal interaction occurs can be determined.

2. Methods

To examine the existence of thermal interaction among multiple boreholes and their possible negative effects on the design performance of the existing nearby boreholes, the transient conduction of heat in the soil surrounding these systems needs to be studied in order to evaluate the temperature rise and the heat flows in the soil surrounding the boreholes. Representation of heat flows to and from the system based in this simulation can serve as inputs into large scale ground water models.

A three-dimensional model of transient conduction of heat in the soil around multiple ground heat exchangers is presented in this section. A domain consisting of two vertical borehole heat exchangers having a distance of $2h$ from each other is considered (Figure 1a). The heat transfer symmetry about the two vertical planes shown in Figure 1a is utilized. Therefore, only one fourth of the borehole field is modelled and the solution domain (soil) is enclosed by the far-field, the ground surface and two symmetry planes. In Figure 1b, the gray area is the solution domain, the results of which can be replicated to the other areas drawn with dashed lines due to their symmetry.

Figure 1. Two-dimensional view of the solution domain: **(a)** horizontal cross sections (xy) at the borehole mid-length ($z=0$ m); **(b)** vertical cross section (xz).



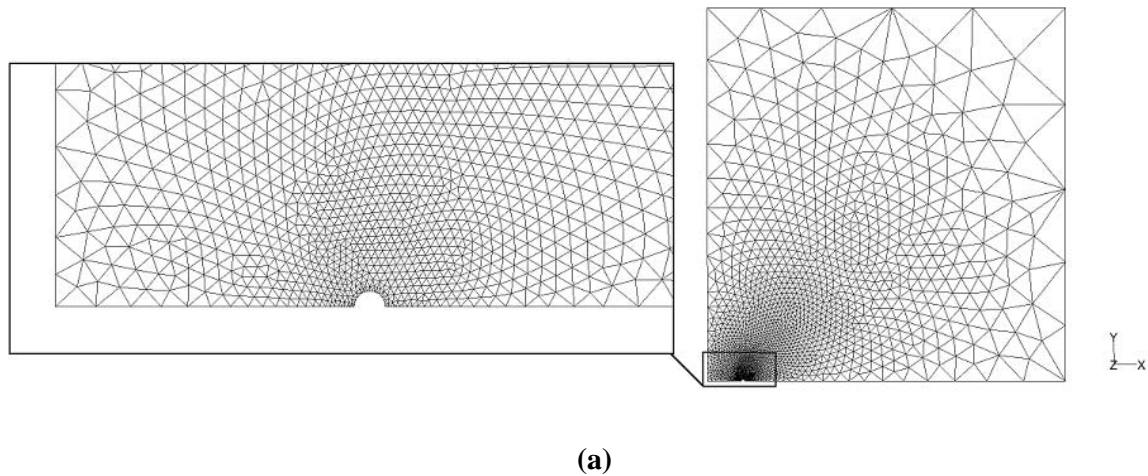
It is assumed that the dominant mode of heat transfer in the soil is conduction. The general heat conduction equation in cylindrical coordinates appears in the following form:

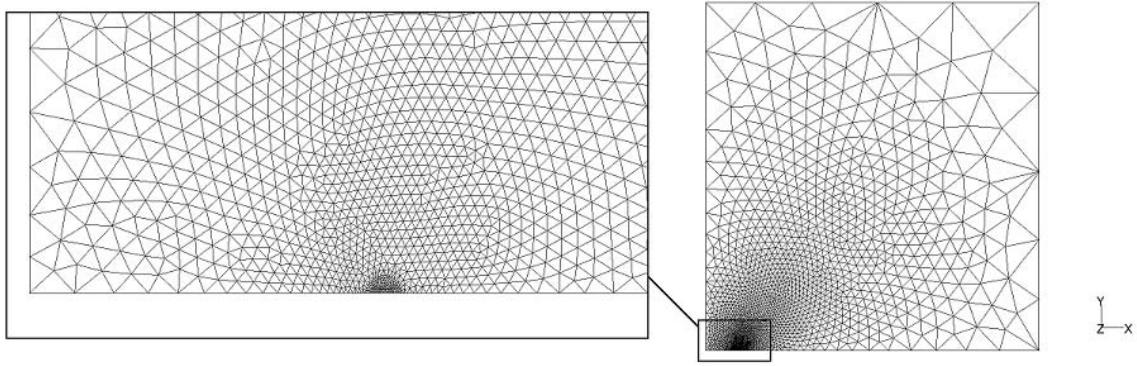
$$\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \varphi^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}_{gen}}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t} \quad (1)$$

where t is the time from the start of operation, α is the thermal diffusivity of soil, and T is the temperature of the ground. The first two terms on the left side of Eq. (1) are the heat flux components in the radial (r) direction, the third and the fourth terms are related to the circumferential (φ) and axial (z) directions, respectively, and the fifth term relates to the heat generated in the control volume. The right side of Eq. (1) represents the transient effects of heat conduction. In the analysis, a numerical approach is used to calculate the temperature profiles of the soil around the boreholes. In the numerical approach, the transient governing integral equations for the conservation of energy is solved with a control volume method in FLUENT. Unlike many of the studies on the heat transfer around multiple boreholes, the current three-dimensional numerical solution takes into account the temperature gradients in the direction adjacent to the borehole length corresponding to the axial heat transfer effects in the soil.

A control-volume-based technique is used that divides the domain into discrete control volumes using unstructured computational triangular grids, as shown in Figure 2. The temperature gradient in the domain between the borehole wall and the farfield changes gradually from large to small ones. Therefore, to reduce computer memory and computational time, the size of the mesh cells is chosen based on this gradual change. The vertical section domain may be discretized using structured grids due to relatively simple geometric structure, as shown in Figure 3.

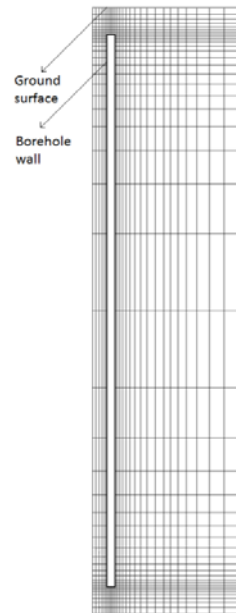
Figure 2. Simulation model for horizontal cross sections (xy) at **(a)** the ground surface ($z=110$ m), and **(b)** borehole mid-length ($z=0$ m).





(b)

Figure 3. Simulation model for multiple boreholes in vertical cross section (xz).



The discretisation in unstructured meshes can be developed from the basic control volume technique where the integral form of the energy conservation equation is used as the starting point:

$$\int_{CV} \text{div}[\text{grad}(T)] dV = \int_{CV} \frac{1}{a} \frac{\partial T}{\partial t} dV \quad (2)$$

Here, ΔV is the volume. Integration of Eq. (2) over a time interval from t to $t + \Delta t$ gives:

$$\int_t^{t+\Delta t} \int_{CV} \text{div}[\text{grad}(T)] dV dt = \int_t^{t+\Delta t} \int_{CV} \frac{1}{a} \frac{\partial T}{\partial t} dV dt \quad (3)$$

Using a fully implicit formulation, Eq. (3) is discretized in the following form:

$$a_p T_p = \sum_{\text{all surfaces}} a_{nb} T_{nb} + a_p^0 T_p^0 \quad (4)$$

where a_p , a_p^0 and a_{nb} are temperature coefficients which are calculated based on the geometric characteristics of each control volume and the time step in the numerical solution.

Equation (4) is solved iteratively at each time level before moving to the next time step to yield updated values of temperature.

Initial and boundary conditions: A uniform initial temperature of 288 K (equal to the undisturbed ground temperature) is assumed to be effective over the entire borefield. At the outer edge of the domain, a constant far-field temperature condition equal to the initial temperature is applied (288 K). The temperature and heat flux distributions on the borehole wall cannot be decided due to the dynamic nature of the heat exchange process between the pipes in the borehole and the borehole wall. However, to simplify the current model, a constant heat flux of 10 W/m^2 on the borehole wall can be assumed since in order to study the thermal interaction between multiple boreholes, their inner dynamic heat exchange process can be of second priority compared to the heat dissipation in the soil surrounding them. As a second approach, a variable heat flux (VHF) along the borehole is calculated by defining the temperature profiles of the fluid running along the pipes in the borehole.

A quasi-three-dimensional model was proposed by Zeng et al. [1,31] taking into account the fluid axial convective heat transfer and thermal “short-circuiting” among U-tube legs. Being minor in order, the conductive heat flow in the grout and ground in the axial direction, however, is still neglected to keep the model concise and analytically manageable. The energy balance equations for up-flow and down-flow of the circulating fluid can be written as

$$\begin{aligned} -\dot{m}c_p \frac{dT_{f1}}{dz} &= \frac{T_{f1} - T_b}{R_1^\Delta} + \frac{T_{f1} - T_{f2}}{R_{12}^\Delta} \\ \dot{m}c_p \frac{dT_{f2}}{dz} &= \frac{T_{f2} - T_b}{R_2^\Delta} + \frac{T_{f2} - T_{f1}}{R_{12}^\Delta} \end{aligned} \quad (0 \leq z \leq H) \quad (5)$$

The following boundary conditions are applied to the governing equations:

$$\begin{aligned} z = 0, \quad T_{f1} &= T_f' \\ z = H, \quad T_{f1} &= T_{f2} \end{aligned} \quad (6)$$

where T_f' is the temperature of the fluid entering the U-tube and

$$R_1^\Delta = \frac{R_{11}R_{22} - R_{12}^2}{R_{22} - R_{12}}, \quad R_2^\Delta = \frac{R_{11}R_{22} - R_{12}^2}{R_{11} - R_{12}}, \quad \text{and} \quad R_{12}^\Delta = \frac{R_{11}R_{22} - R_{12}^2}{R_{12}} \quad (7)$$

where R_{11} and R_{22} are the thermal resistance between the circulating fluid and the borehole wall, and R_{12} is the resistance between the pipes. In most engineering practice, the configuration of the U-tube in the borehole may be assumed symmetric, and here it is assumed that $R_{11}=R_{22}$. The steady-state conduction problem in the borehole cross-section was analyzed in detail by Hellström [4] with the line source and multiple approximations. The line-source assumption results in the following solution:

$$\begin{aligned} R_{11} &= \frac{1}{2\pi k_b} \left[\ln\left(\frac{r_b}{r_p}\right) + \frac{k_b - k}{k_b + k} \cdot \ln\left(\frac{r_b^2}{r_b^2 - D^2}\right) \right] + R_p \\ R_{12} &= \frac{1}{2\pi k_b} \left[\ln\left(\frac{r_b}{2D}\right) + \frac{k_b - k}{k_b + k} \cdot \ln\left(\frac{r_b^2}{r_b^2 + D^2}\right) \right] \end{aligned} \quad (8)$$

where r_b , k_b , k , D and R_p are the radius of the boreholes, the grout thermal conductivity, the soil thermal conductivity, the distance between the pipes in the borehole, and the thermal resistance of conduction in the pipe, respectively.

Zeng et al. [1] formulated the temperature profiles of the fluids running in the U-pipes in the boreholes:

$$\begin{aligned}\Theta_1(Z) &= \cosh(\beta Z) - \frac{1}{\sqrt{1-P^2}} \left[1 - P \frac{\cosh(\beta) - \sqrt{\frac{1-P}{1+P}} \sinh(\beta Z)}{\cosh(\beta) + \sqrt{\frac{1-P}{1+P}} \sinh(\beta)} \right] \cdot \sinh(\beta Z) \\ \Theta_2(Z) &= \frac{\cosh(\beta) - \sqrt{\frac{1-P}{1+P}} \sinh(\beta)}{\cosh(\beta) + \sqrt{\frac{1-P}{1+P}} \sinh(\beta)} \cosh(\beta Z) + \frac{1}{\sqrt{1-P^2}} \left[\frac{\cosh(\beta) - \sqrt{\frac{1-P}{1+P}} \sinh(\beta)}{\cosh(\beta) + \sqrt{\frac{1-P}{1+P}} \sinh(\beta)} - P \right] \cdot \sinh(\beta Z)\end{aligned}\quad (9)$$

where the dimensionless parameters are defined as

$$\begin{aligned}\Theta &= \frac{T_f(z) - T_b}{T'_f - T_b}, \quad Z = \frac{z}{H}, \quad P = \frac{R_{12}}{R_{11}} \\ \beta &= \frac{H}{\dot{m} c_p \sqrt{(R_{11} + R_{12})(R_{11} - R_{12})}}\end{aligned}\quad (10)$$

The heat transferred to the soil from each of the pipes in the borehole can be obtained from Eq. (1). In this equation we only take the first term on the right hand side.

$$q''(z) = \frac{T_{f1}(z) - T_b}{R_1^\Delta} + \frac{T_{f2}(z) - T_b}{R_2^\Delta}\quad (11)$$

Using the dimensionless parameters introduced in Eq. (10), Eq. (11) can be rewritten in terms of the dimensionless parameters:

$$q''(Z) = (T'_f - T_b) \left[\frac{\Theta_1(Z)}{R_1^\Delta} + \frac{\Theta_2(Z)}{R_2^\Delta} \right]\quad (12)$$

Assuming that the heat is dissipated symmetrically in the soil around each borehole, Eq. (12) can be written in the following form:

$$q'(Z) = \pi D_b (T'_f - T_b) \left[\frac{\Theta_1(Z)}{R_1^\Delta} + \frac{\Theta_2(Z)}{R_2^\Delta} \right]\quad (13)$$

This is the spatial distribution of the heating strength along the rod. In contrast to past studies, this heating strength varies along the rod and is not constant. Note that the variable heat source model has made certain simplifying assumptions, such as constant ground temperature.

In order to compare the results gained by constant heat flux model with the results gained by the VHF model, an equivalent inlet temperature ($T'_f = 297.7K$) for the VHF model, resulting in the same total heat conduction in the soil, is assumed. In addition, to account for the transient term in Eq. (1), the time is subdivided into 4200 time steps of 3600 s which equals a time period of 6 months.

3. Results and Discussion

In the current study, typical geometrical and thermal characteristics for the borehole and the surrounding soil are assumed (Table 1). Note that the properties of soil are approximate values for dry clay.

Table 1. Parameters of the reference borehole

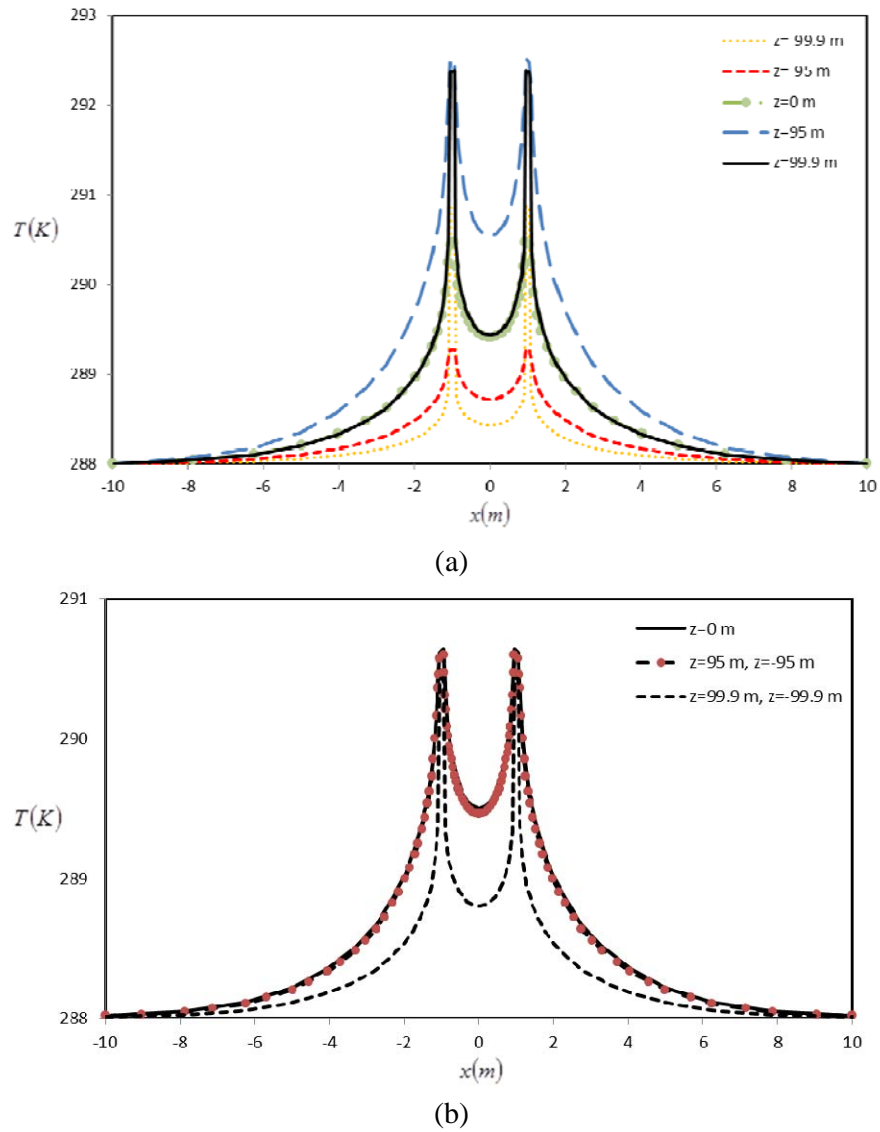
(a) Inside the borehole (pipe and grout region)									
H (m)	r_b (m)	r_p (m)	D (m)	D_b (m)	β	P	k_b (W/mK)	\dot{m} (kg/s)	c (J/kgK)
200	0.05	0.02	0.02	2	1.8	0.3	1	0.2	4187

(b) Outside the borehole (soil region)		
k (W/mK)	c_p (J/kgK)	ρ (kg/m ³)
1	1381	1200

The temperature responses of the soil around multiple boreholes evaluated by the VHF model at various borehole depths are compared in Figure 4a. It is shown that the maximum temperature rise due to thermal interaction of multiple boreholes in a six-month period of heat transfer from the borehole into the soil occurs at the top 3% heating length of the borehole ($z=95$ m) and it decreases along the borehole length as the heat flux from the borehole wall into the soil decreases. Therefore, with the objective of limiting boreholes' operations and sizes in order to prevent their thermal interaction, the top length of the boreholes (about 3% total length) is the critical area. The thermal interaction between the boreholes is at its minimum at the bottom of the borehole ($z=-100$ m) where the heat flux to the soil is lowest. This is not true for the case of constant heat flux from the borehole wall to the surrounding soil along the borehole length (Figure 4b). It is seen in Figure 4b that the greatest thermal interaction occurs at top of the borehole, but remains at its maximum amount along the borehole length. For this case, the critical length of the borehole would be almost 95% of the borehole length. However, as discussed earlier, the case of constant heat flux is only a simplification to the VHF problem and does not present the problem as accurate as the VHF problem.

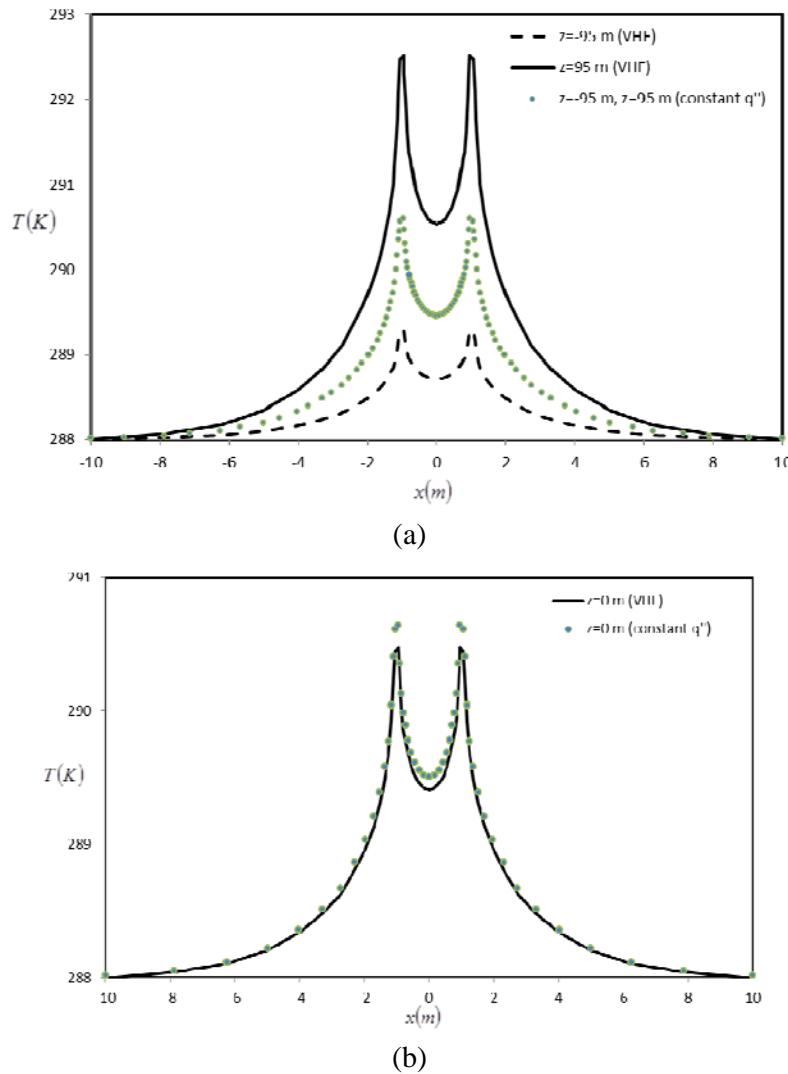
Another notable characteristic of Figures 4a and 4b is the decrease in the thermal interaction in the lengths of $z=99.5$ m when one moves from $z=95$ m towards the top end of the borehole. Specifically for the case of VHF (Figure 4a), there is higher heat flux as one moves towards the top end and one expects greater thermal interactions. In both cases, the decrease in the temperature rise in the soil around the borehole declines at the very end of borehole length, and this can be due to axial heat transfer effects which become notable only at the very ends of borehole lengths.

Figure 4. Soil temperature (K) around multiple boreholes in $t = 6$ months, at various borehole depths for (a) VHF model, and (b) constant heat flux model.



The results of the VHF model and constant heat flux model are compared in Figure 5. It is seen in Figure 5a that the assumption of constant heat flux on the borehole wall introduces numerous inaccuracies especially when dealing with the temperature rises in the soil at the very top and bottom of the borehole. Figure 5b shows that, by using the quasi-three-dimensional model for the heat transfer inside the borehole, the heat flux on the borehole is spread along the borehole in a way that the middle area remains similar to its average amount. It can be concluded that using the constant heat flux method is only valid for the middle length of the boreholes and moving any further to the top or bottom of the borehole, the temperature rises evaluated become increasingly inaccurate. Quasi-three-dimensional models reveal drawbacks of two-dimensional models and are thus preferred for design and analysis of ground heat exchangers, as they provide more accurate information for performance simulation and analysis and design.

Figure 5. Comparison of soil temperature (K) around multiple boreholes at $t = 6$ months for VHF and constant heat flux models, at (a) $z=95$ m and $z=-95$ m, and (b) $z=0$ m.



Extension of results to systems of boreholes: The methods used for calculating the temperature profiles in the soil around two boreholes can also be applied to two systems of vertical GHEs. For example, if an area of 40 m x 40 m x 200 m in the soil is occupied for one system of vertical GHEs, the ratio of system depth to its initial size is large enough to be accounted as one cylinder or line source of heat when system interactions and temperature excess around a system with larger distances are to be accounted for. The study of variable heating strength along the borehole length also accounts for the system of boreholes as well. Therefore, the parametric study on two interacting boreholes likely exhibits the same results as those for two interacting systems of boreholes. However, the assumption of constant ground temperature must be examined further in order to improve the accuracy of the proposed method.

4. Conclusions

The performance of multiple boreholes or neighbouring borehole systems and their possible thermal interactions are discussed. The effect of borehole heat flux on the transient response of multiple ground heat exchangers and their thermal interaction is described. In addition, a quasi-three-dimensional model for heat transfer inside the borehole is utilised as the boundary condition for the three-dimensional transient heat transfer analysis outside the borehole in order to evaluate the temperature rise in the soil surrounding multiple boreholes and their interaction. It is shown that the maximum temperature rise due to thermal interaction of multiple boreholes in a six-month period of heat transfer from the borehole into the soil occurs right after the beginning of the borehole (about 3% total length) and it decreases along the borehole length as the heat flux from the borehole wall into the soil decreases. Therefore, with the objective of limiting boreholes' operations and sizes in order to prevent their thermal interaction, the top length of the boreholes is the critical area. It can be concluded that using the constant heat flux method is only valid for the middle length of the boreholes and moving any further to the top or bottom of the borehole, the temperature rise evaluations become increasingly inaccurate.

Nomenclature

a	temperature coefficient
c_p	specific heat at constant pressure [J/kgK]
D	distance between the pipes in the borehole [m]
D_b	distance between the boreholes [m]
h	borehole distance from the coordinate centre [m]
H	heating length
k	soil thermal conductivity [W/mK]
k_b	grout thermal conductivity [W/mK]
\dot{m}	mass flow rate [kg/s]
P	dimensionless parameter (Eq. (9))
\dot{q}	generated heat per unit volume [W/m ³]
q''	heat flux at borehole wall [W/m ²]
r	radial coordinate [m]
r_p	pipe radius [m]
r_b	borehole radius [m]
R_{11}	thermal resistance between the inlet circulating fluid and the borehole wall [mK/W]
R_{12}	thermal resistance between the inlet and outlet pipes [mK/W]
R_{22}	thermal resistance between the outlet circulating fluid and the borehole wall [mK/W]
R_1^Δ	dimensionless thermal resistance (Eq. (7))
R_{12}^Δ	dimensionless thermal resistance (Eq. (7))
R_2^Δ	dimensionless thermal resistance (Eq. (7))
R_p	thermal resistance of conduction in the pipe [mK/W]
T	temperature [K]

T'_f	inlet circulating fluid temperature at $z=100$ m
t	time [s]
V	volume [m^3]
Z	dimensionless parameter (Eq. (9))
z	axial coordinate [m]

Greek Letters

α	thermal diffusivity [m^2/s]
β	dimensionless parameter (Eq. (9))
Θ	dimensionless temperature (Eq. (8))
φ	circumferential coordinate [rad]
ρ	density [kg/m^3]

Subscripts

nb	node number of the adjacent cell
P	centroid P

Superscripts

0	previous time step
$f1$	inlet circulating fluid
$f2$	outlet circulating fluid
n	discretization step designation in time

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Conflict of Interest

The authors declare no conflict of interest.

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