Exhausted olive pomace phenolic-rich extracts obtention, a first step for a biorefinery scheme proposal







Irene Gómez-Cruz¹, Inmaculada Romero¹, María del Mar Contreras¹, Carmen Padilla-Rascón¹, Florbela Carvalheiro², Luis C. Duarte², Luisa B. Roseiro²

¹Department of Chemical, Environmental and Materials Engineering, Universidad de Jaén, Jaén, Spain; <u>igcruz@ujaen.es</u> (I.G.-C.); <u>iromero@ujaen.es</u> (I.R.); <u>mcgamez@ujaen.es</u> (M.D.M.C.); <u>cpadilla@ujaen.es</u> (C.P.-R.) ²Unidade de Bioenergia e Biorrefinarias, LNEG – Laboratório Nacional de Energia e Geologia, Lisbon, Portugal; <u>florbela.carvalheiro@lneg.pt</u> (F.C.); <u>luis.duarte@lneg.pt</u> (L.C.D.); <u>luisa.roseiro@lneg.pt</u> (L.B.R.)







- \succcurlyeq Introduction
- \succcurlyeq Objective
- Material and Methods
 Raw material
 Experimental conditions
- オ Results
- \succcurlyeq Conclusions
- ➢ References and acknowledgments



INTRODUCTION



- **Spain** is the world's leading producer and exporter of olive oil
- 2.5 million ha of olives are cultivated in Spain
- Olive oil production generates every year 4.2 million tons/year of residues [1]
- (see scheme) and there by it is a big deal for the Spanish industry.



Scheme production of olive oil and waste generated (orange squares)



INTRODUCTION



Nowadays, an increasing demand on natural antioxidants exists by both consumers and industry. These compounds

can replace synthetic antioxidants that have some side effects.





INTRODUCTION





biorefinery based on olive biomass

- Nowadays, the development of a biorefinery that contributes to the integral use of the resources of the olive grove is valued as of great social, environmental, and economic interest.
- Among these sources, exhausted olive pomace (EOP) is considered a promising feedstock within the context of biorefinery for the production of bioenergy and valuable chemicals, including natural antioxidants.
- The latter use can provide with an extra income to the current application of EOP as a low-cost fuel for domestic and industrial heating.







The aim of this work was to obtain antioxidants from EOP. The extraction experiments to achieve this objective are:

Ultrasound-assisted extraction (UAE) was performed using sequential extraction with water and
 70% acetone as solvents.

UAE is considered an efficient extraction technique

- Reduces extraction time
- Reduces solvent and energy consumption

Benefits

- Increasing yields
- Savings on an industrial scale

2) Maceration using water at 85 °C under agitation.



MATERIAL AND METHODS



Raw material and chemical composition

- Olive pomace industry "Spuny SA" (Castellar, Jaén)
- Pitted and pelletized



- Extractives
- Acid Insoluble Lignin (AIL)
- Acid Soluble Lignin (ASL)
- Carbohydrates
- Acetyl groups

• Ash

Experimental conditions

Extraction method	Solvent	Time (min)	Temperature (ºC)	Solids (%)
UAE	Water	30	30	10
UAE	70% acetone	30	30	10
Maceration	Water	90	85	10





RESULTS



EOP chemical composition



- The chemical composition of EOP was: 41.8% of extractives, 20.6% of carbohydrates and 21.8% of lignin.
- Since the major component are **extractives**, its valorization is crucial.
- Thereby, the antioxidant fraction of the extractives was obtained by different methods as a first step for the valorization of EOP.



RESULTS



Total phenolic content and antioxidant activity of the liquid extracts

Extraction method	Solvent	Sample	TPC g GAE/L	DPPH g TE/L	ABTS g TE/L
UAE	Water	Extract 1	1.37 ± 0.01	1.38 ± 0.09	3.43 ± 0.05
UAE	70% acetone	Extract 2	1.01 ± 0.06	0.98 ± 0.05	1.50 ± 0.12
		Extract 3	0.50 ± 0.03	0.50 ± 0.01	0.99 ± 0.05
		Mixture	0.96 ± 0.03	0.98 ± 0.01	1.94 ± 0.01
		Extract 1	1.28 ± 0.03	1.54 ± 0.01	3.43 ± 0.04
		Extract 2	0.83 ± 0.09	0.90 ± 0.03	1.91 ± 0.05
		Extract 3	0.77 ± 0.00	0.55 ± 0.02	0.83 ± 0.11
		Mixture	0.97 ± 0.01	1.00 ± 0.07	2.04 ± 0.03
Maceration	Water	Extract	4.22 ± 0.1	3.04 ± 0.27	6.77 ± 0.47

- Using 10% solids load and UAE at 30 °C, it is recommended to perform three sequential extractions in order to recover the highest possible concentration of phenolic compounds.
- Using water extraction through maceration at 80 °C, higher amounts of phenolic compounds were solubilized in the liquid fraction in a single step; i.e., 4.22 GAE vs. 2.88 GAE using UAE with both solvents if the extracts were dried.







Total phenolic content and antioxidant activity of the liquid extracts



- When the results were expressed in terms of extract, UAE with water-acetone revealed to be more effective than with water; 95.7 versus 74.4 mg GAE/g extract, respectively.
- This can be explained due to the amounts of solids was higher using the latter methods, reducing the purity of the extract.
- The extract obtained in an agitated water bath at 85 °C showed a TPC of 65.9 mg GAE/g extract.
- The antioxidant activity of the extracts revealed to be in accordance with the TPC, being the results higher for UAE extracts, particularly, using water-acetone.





Phenolic profile of the water-acetone extract



COOH 7.027 Norm. 99.9% Hydroxytyrosol 98.7% 3-HBA 600 500 400 98.5% Pinoresinol 98.7% Catechol 300 4.860 8.750 200 98.3% Oleuropein 467 derivative 799 5.849 99.5% Tyrosol 100 10 min

- The electrophoretic analysis revealed the presence of hydroxytyrosol as major compound of the extract.
- This agreed with other studies that found hydroxytyrosol in olive pomace (OP).
- Remarkably, our results suggest that this compound is highly resistant since OP is subjected to drying and solvent extraction to recover the olive pomace, obtaining EOP as final waste.
- Electropherograms at 200 nm of the water-acetone extract obtained by UAE





- The electrophoretic profile was similar to the aqueous extract and the major compound of the extract was again hydroxytyrosol.
- This can be explained due to its high polarity being extracted by water and its mixture with acetone.



CONCLUSIONS



Results showed that EOP presents a significant amount of phenolic compounds, independently of the extraction conditions.

While the highest solubilization of phenolic compounds was obtained using water extraction at 80 °C, UAE with 70% acetone revealed to be more effective for the obtention of an extract richer in antioxidants.

Hydroxytyrosol was the major compound found in all the extracts, which is also considered one of the most powerful antioxidants.

EOP is a promising source of added-value phenolic compounds with antioxidant activity, in particular hydroxytyrosol, and its obtention is worth-merit before the exploration of this waste for bioenergy production.



REFERENCES AND AKNOWLEDGMENTS



References

- Manzanares, P.; Ruiz, E.; Ballesteros, M.; Negro, MJ.; Gallego, FJ.; López-Linares, JC.; Castro, E. Residual biomass potential in olive tree cultivation and olive oil industry in Spain valorization proposal in a biorefinery context. Spanish journal of agricultural research **2017**,15,3.

- European Commission Commission Regulation (EU) No 1018/2013 of 23 October 2013 amending Regulation (EU) No 432/2012 establishing a list of permitted health claims made on foods other than those referring to the reduction of disease risk and to children's development and health. *Off. J. Eur. Union L 282.* **2013**, *56*, 43–45, doi:http://eur-lex.europa.eu/pri/en/oj/dat/2003/I_285/I_28520031101en00330037.pdf.

- Turck, D.; Bresson, J.; Burlingame, B.; Dean, T.; Fairweather-Tait, S.; Heinonen, M.; Hirsch-Ernst, K.I.; Mangelsdorf, I.; McArdle, H.J.; Naska, A.; et al. Safety of hydroxytyrosol as a novel food pursuant to Regulation (EC) No 258/97. *EFSA J.* **2017**, *15*, doi:10.2903/j.efsa.2017.4728.

Acknowledgments:

- Financial support from Agencia Estatal de Investigación and Fondo Europeo de Desarrollo Regional. Reference project ENE2017-85819-C2-1-R.
- Irene Gómez-Cruz expresses her gratitude to the Universidad de Jaén for financial support (grant R5/04/2017).
- Authors also thank the FEDER UJA projects 1260905 funded by "Programa Operativo FEDER 2014-2020" and "Consejería de Economía y Conocimiento de la Junta de Andalucía".

THANK YOU FOR YOUR ATTENTION







Irene Gómez-Cruz¹, Inmaculada Romero¹, María del Mar Contreras¹, Carmen Padilla-Rascón¹, Florbela Carvalheiro², Luis C. Duarte², Luisa B. Roseiro²

¹Department of Chemical, Environmental and Materials Engineering, Universidad de Jaén, Jaén, Spain; <u>igcruz@ujaen.es</u> (I.G.-C.); <u>iromero@ujaen.es</u> (I.R.); <u>mcgamez@ujaen.es</u> (M.D.M.C.); <u>cpadilla@ujaen.es</u> (C.P.-R.) ²Unidade de Bioenergia e Biorrefinarias, LNEG – Laboratório Nacional de Energia e Geologia, Lisbon, Portugal; <u>florbela.carvalheiro@lneg.pt</u> (F.C.); <u>luis.duarte@lneg.pt</u> (L.C.D.); <u>luisa.roseiro@lneg.pt</u> (L.B.R.)