

Effect of Temperature and Steam to Biomass ratio on NO and SO₂ Formation in Palm Kernel Shell Catalytic Steam Gasification with In-situ CO₂ Adsorption

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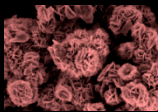
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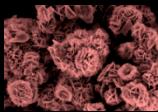
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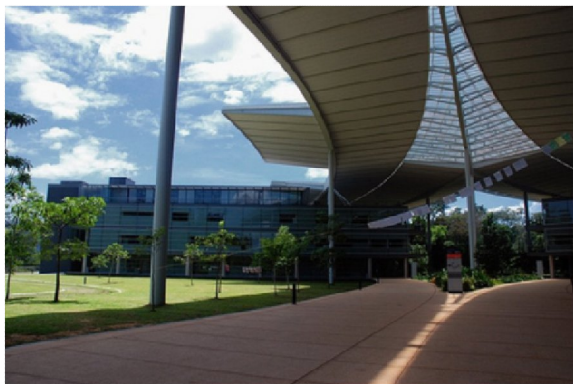


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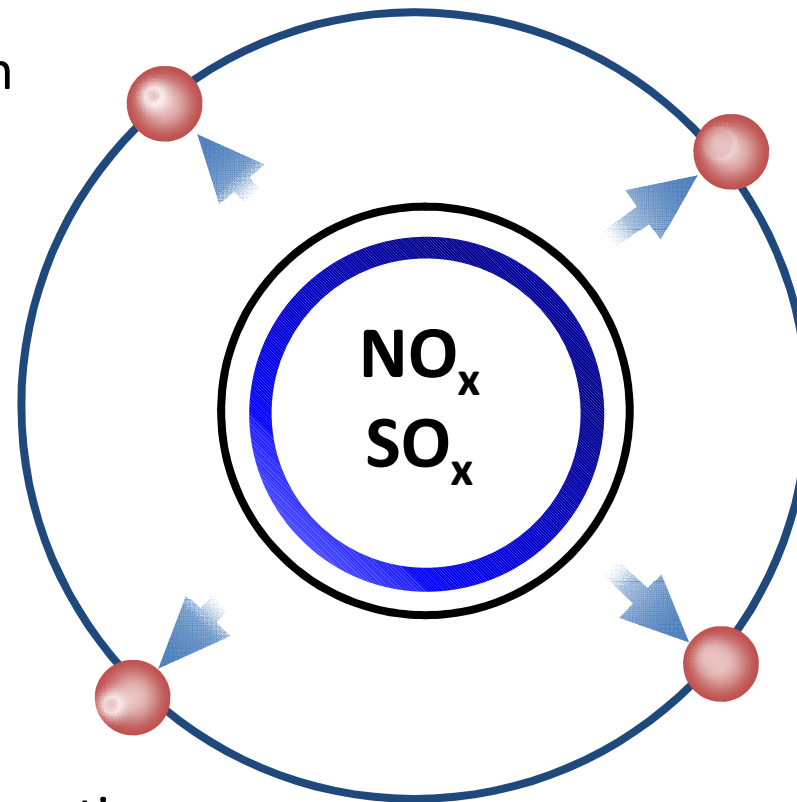
Centre of Biofuel and Biochemical Research (CBBR)
PETRONAS Ionic Liquids Center



Motivation

Effect on
human health

Effect on aquatic and
ecosystem



Acid rain formation

Effect on crops
and infrastructure

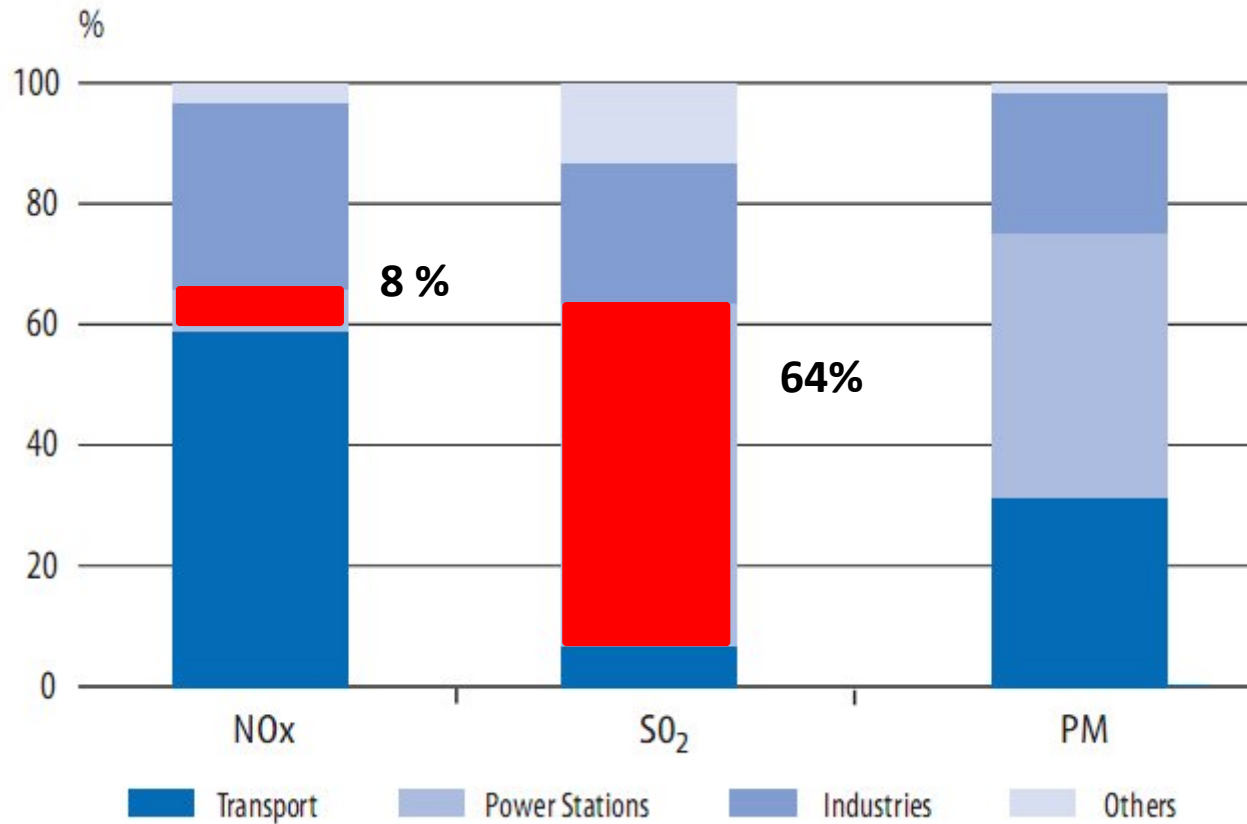
NO_x and SO_x Formation

- Inherent **Nitrogen** and **Sulfur** in biomass convert to **NO** and **SO**
- NO and SO further convert to **NO₂** and **SO₂** if excess oxidizing agent (oxygen) is available

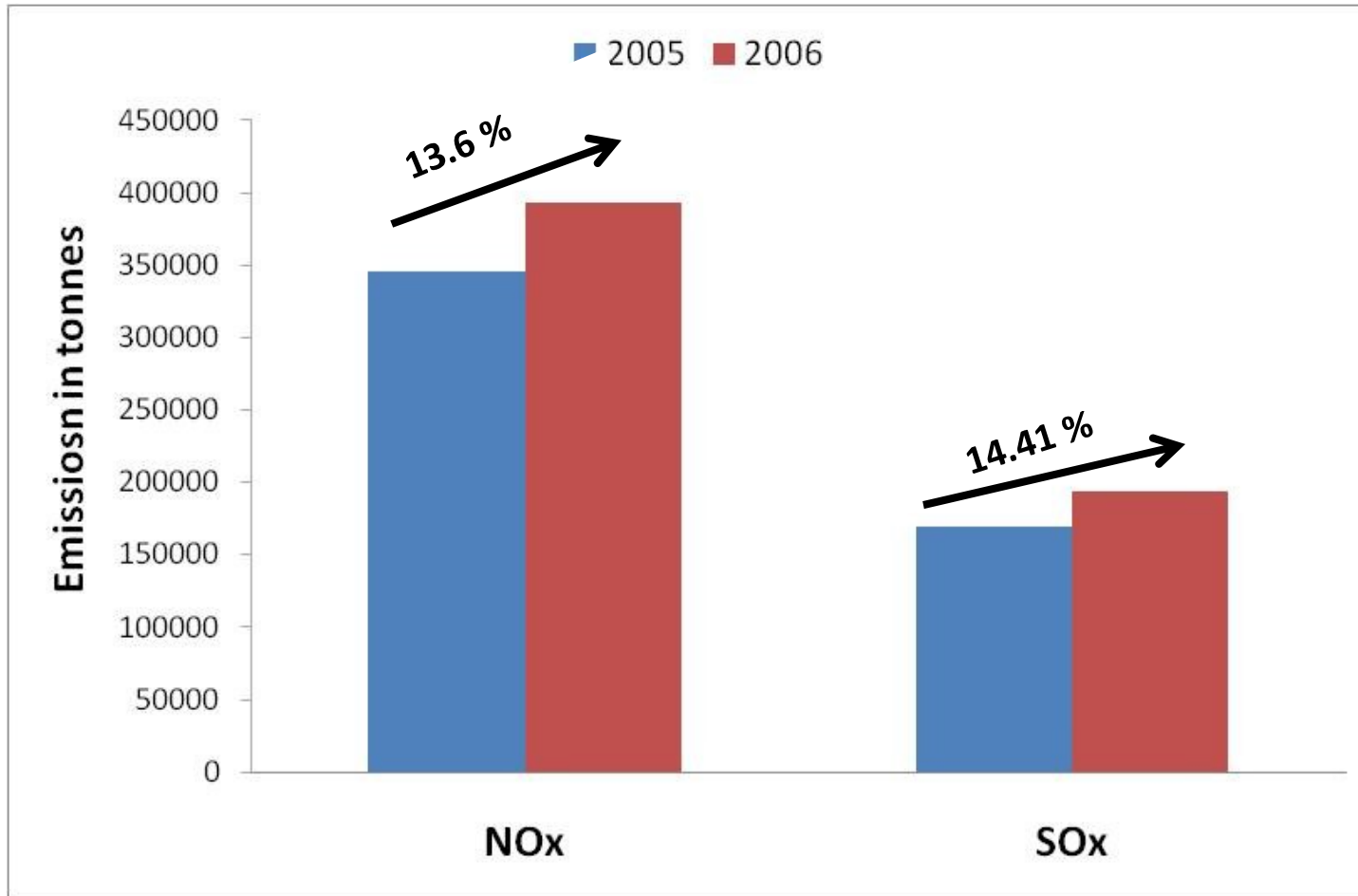
NO and SO₂ emissions are more critical in coal combustion and gasification due to high N and S content

Malaysia-NO_x and SO_x Sources

Emissions in 2004



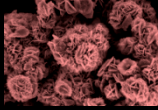
Malaysia-NO_x and SO_x Emissions



Present Study

Effect of Temperature and steam to biomass ratio

- NO formation
- SO₂ formation
- Comparative study with biomass based power plants



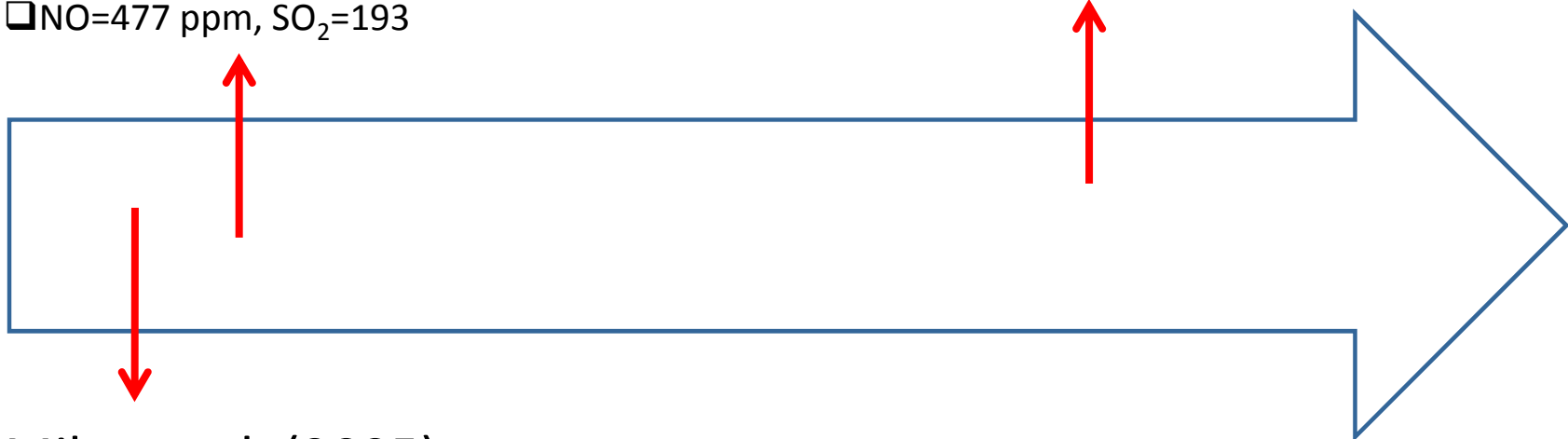
Literature Review

Patel et al. (2001)

- ❑ Poultry litter and coal co-firing steam gasification (
- ❑ T=843 °C (Fixed bed gasifier)
- ❑ NO=477 ppm, SO₂=193

Sethuraman et al. (2010)

- ❑ Wood and Corn air gasification
- ❑ T= 815 °C
- ❑ NO=



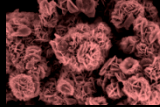
Miles et al. (2005)

- ❑ Swine and turkey litter mixture coal co-firing combustion using CaO
- ❑ T=720 °C
- ❑ NO_x=10-50 ppm, 0-25 ppm

Present study

- ❑ NO and SO₂ formation from biomass catalytic steam gasification with CO₂ adsorbent
- ❑ Temperature 600-750 °C





Biomass Sample Preparation

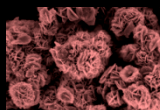
Palm kernel shell

- ❑ Obtained from My 4-Seasons International Sdn. Bhd.
- ❑ Particle diameter range 0.1-4 mm
- ❑ Sieved to particle size of 1.0-2.0 mm



Palm Kernel Shell Properties

Analysis	Wt% (dry basis)
Moisture	9.61
Volatiles	80.92
Ash	4.31
Fixed Carbon (by diff.)	14.67
C	49.74
H	5.68
N	1.02
S	0.27
O (by diff.)	43.36



Catalyst and Adsorbent Preparation

Catalyst

- Ni powder used as commercial catalyst
- Purchased from Merck Chemicals
- Particle diameter $\sim 10\mu\text{m}$

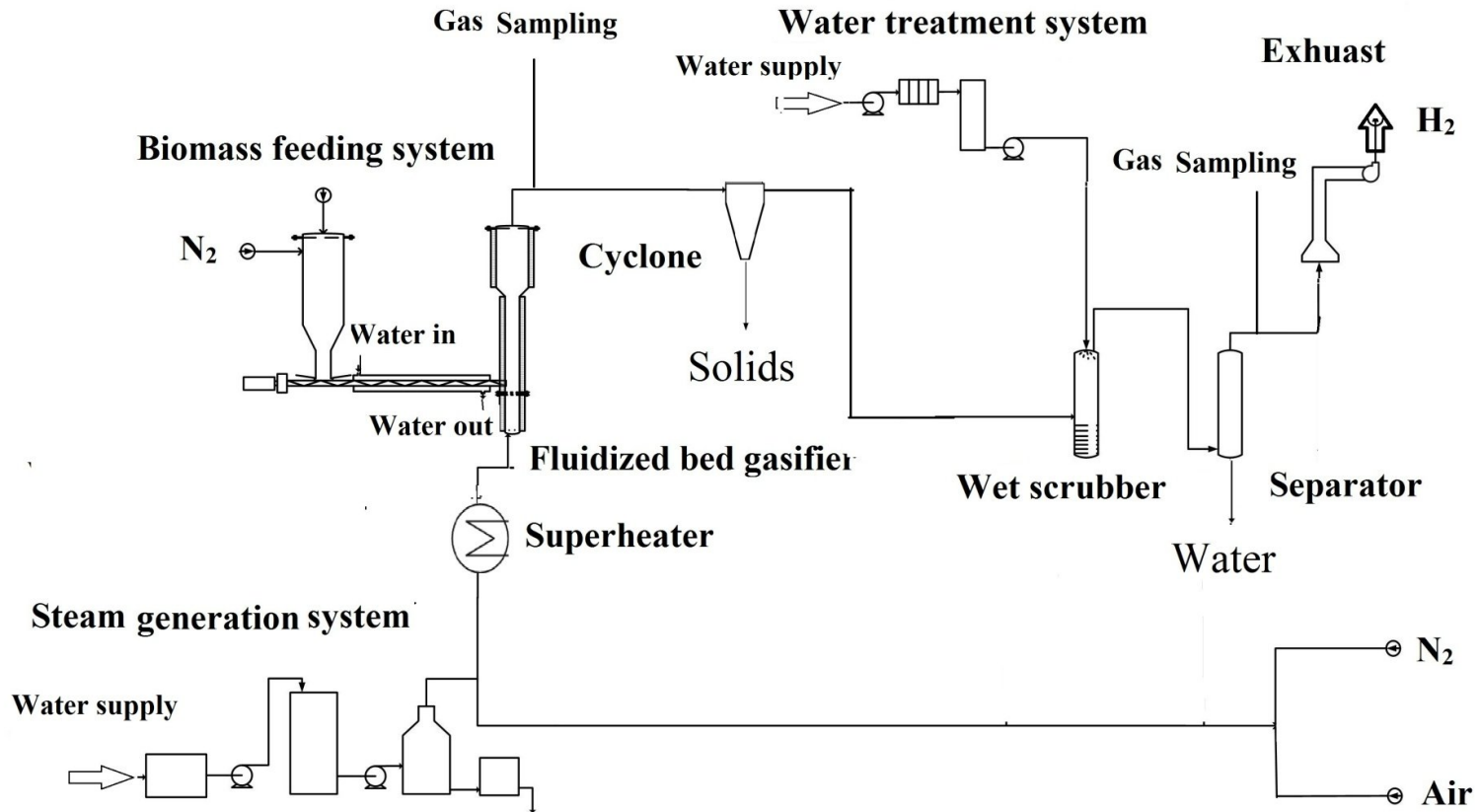
Adsorbent

- Purchased from Universal Lime Sdn. Bhd
- Grinded and sieved to particle size of 150-250 μm

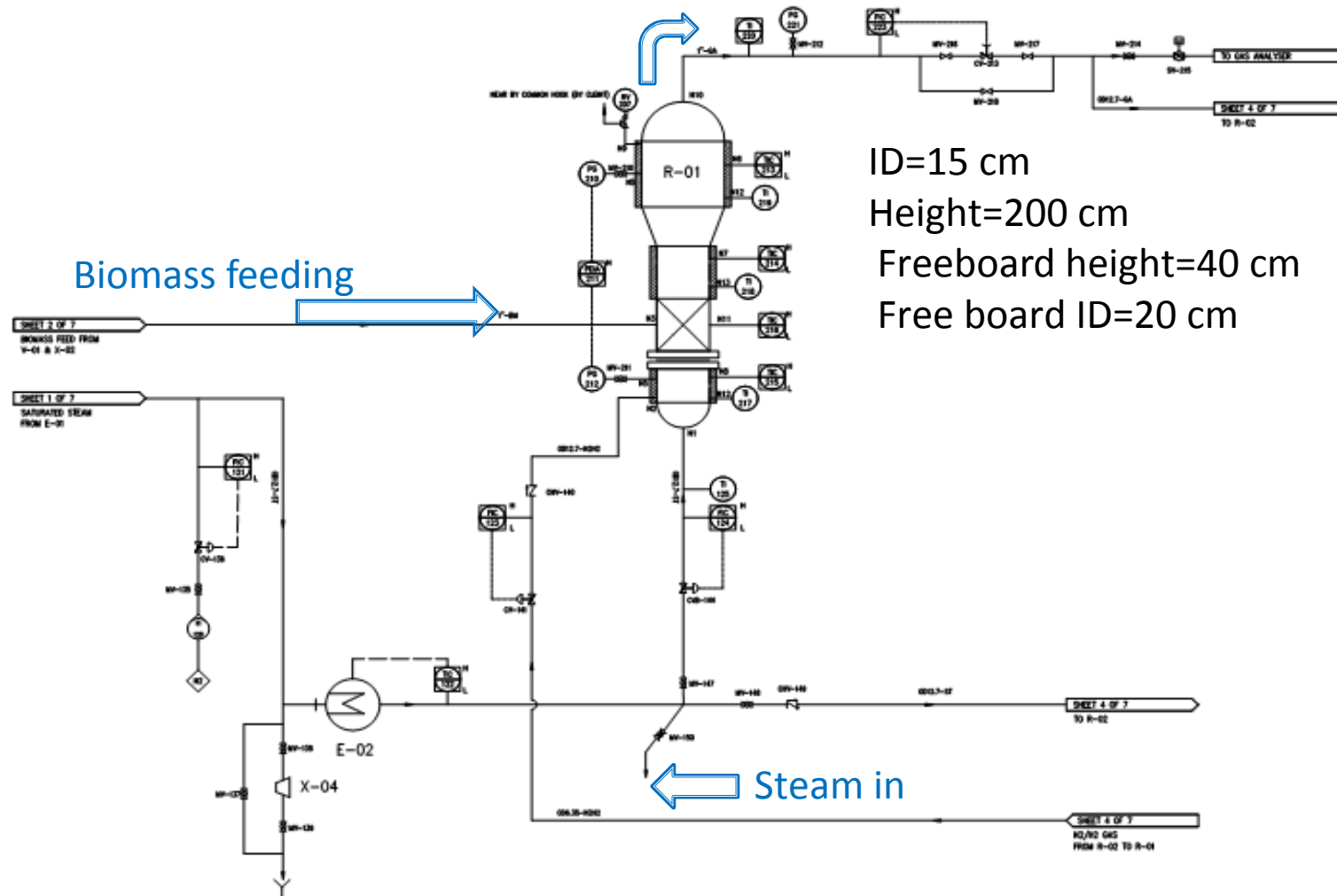
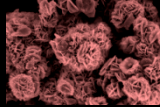
Quicklime	
Particle density	3053 Kg/m ³
Bulk density	1047 Kg/m ³



Experimental Set Up

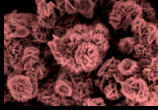


Fluidized Bed Gasifier




Operating Conditions

Parameter	Values
Biomass flow rate (kg/h)	1.35
Fluidized bed temperature (°C)	600, 675, 750
Pressure (atm)	1
Steam to biomass ratio (wt/wt)	1.5, 2.0, 2.5
Catalyst to biomass ratio (wt/wt)	0.1
Adsorbent to biomass ratio (wt/wt)	1.0



Experimental Procedure



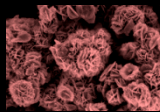
Fluidized bed gasifier with adsorbent heated to their desired temperature

Superheated steam introduced to fluidized bed gasifier at 300 °C from superheater

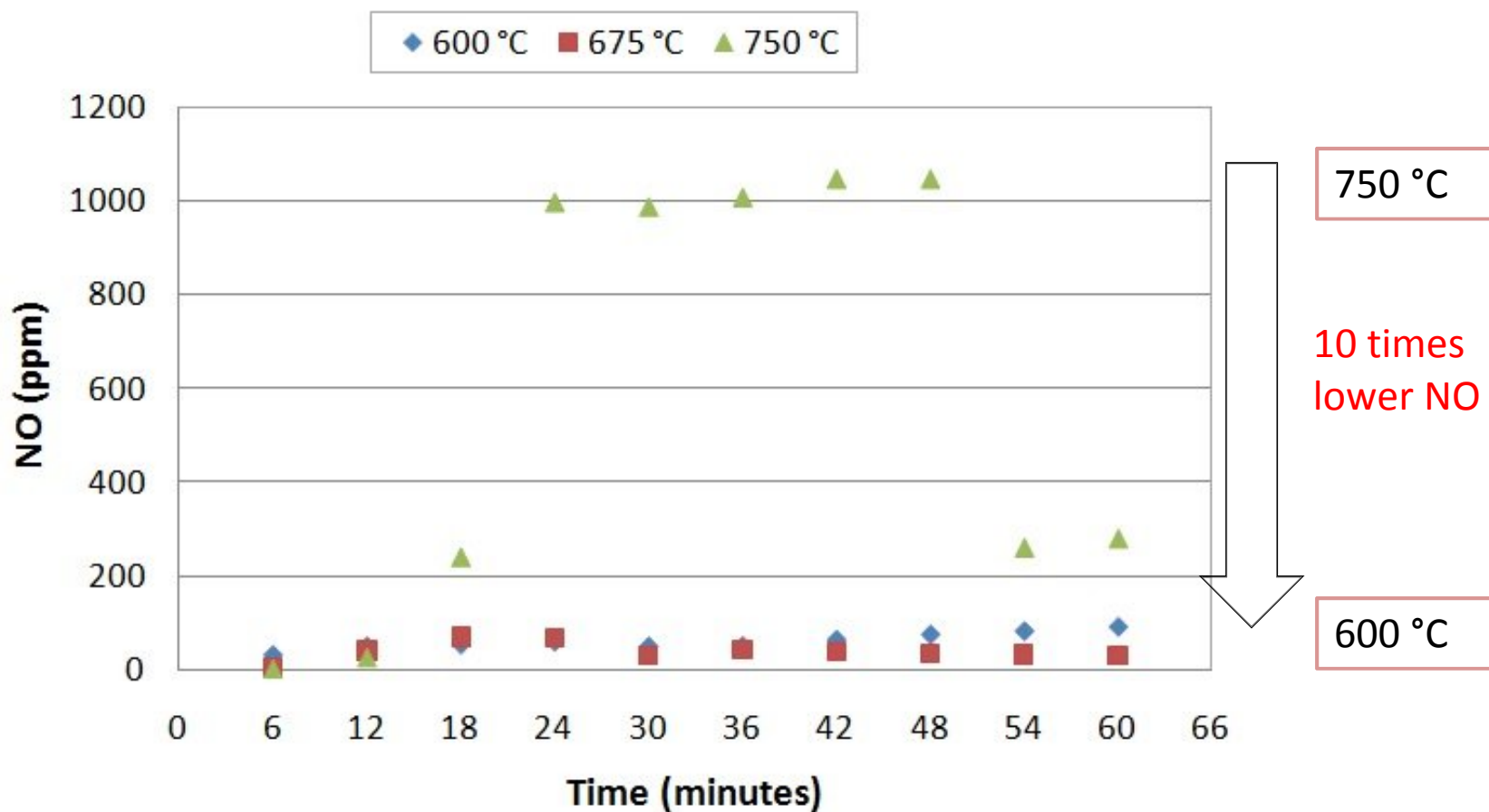
Biomass+ catalyst is introduced when reactor temperature is stabilized

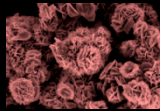
Air is purged into the system after gasification experiment to combust the solid residue remaining in the system to calculate char

Each experiments lasted for 60 minutes

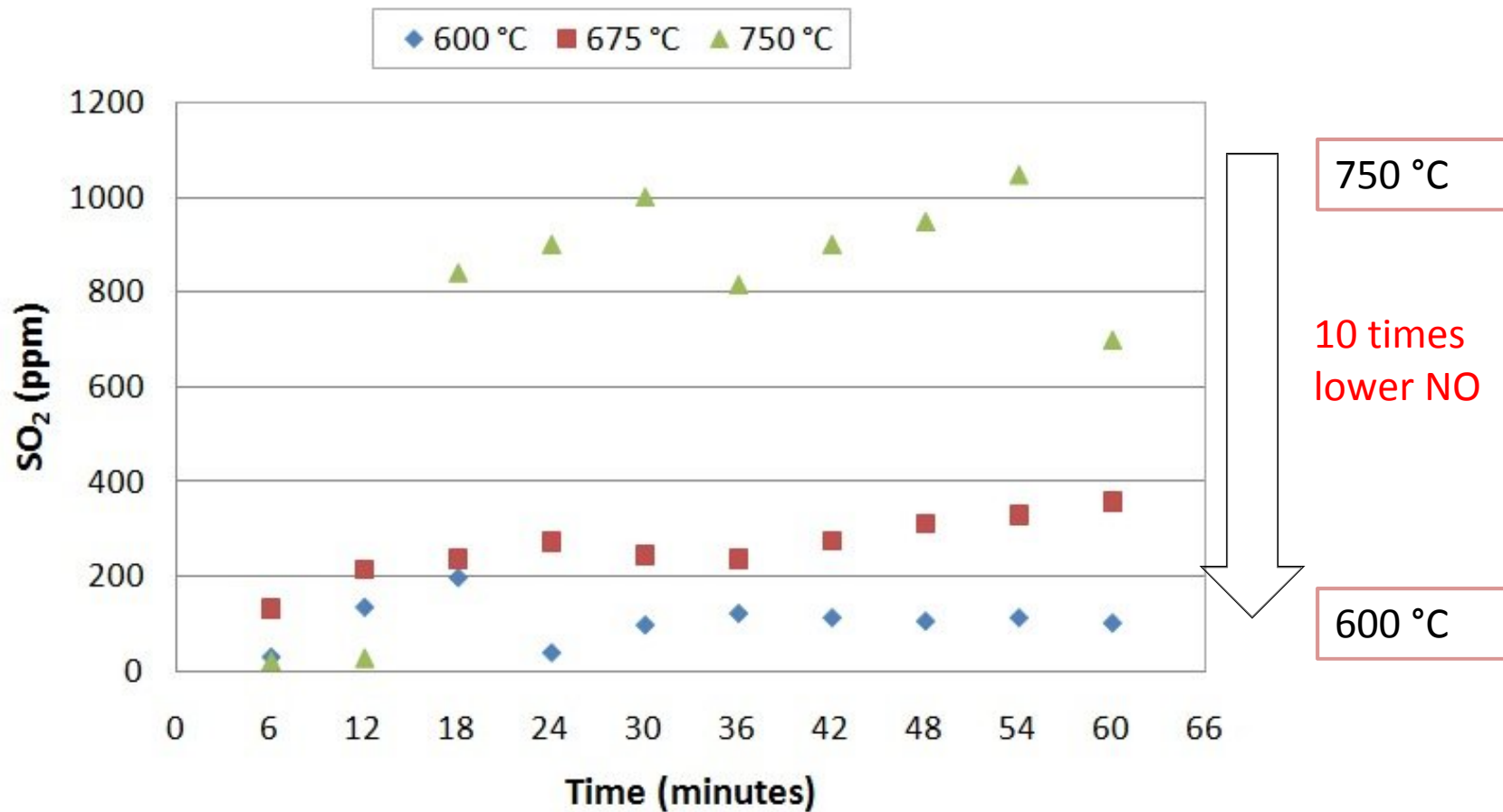


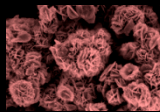
NO Formation-Effect of Temperature





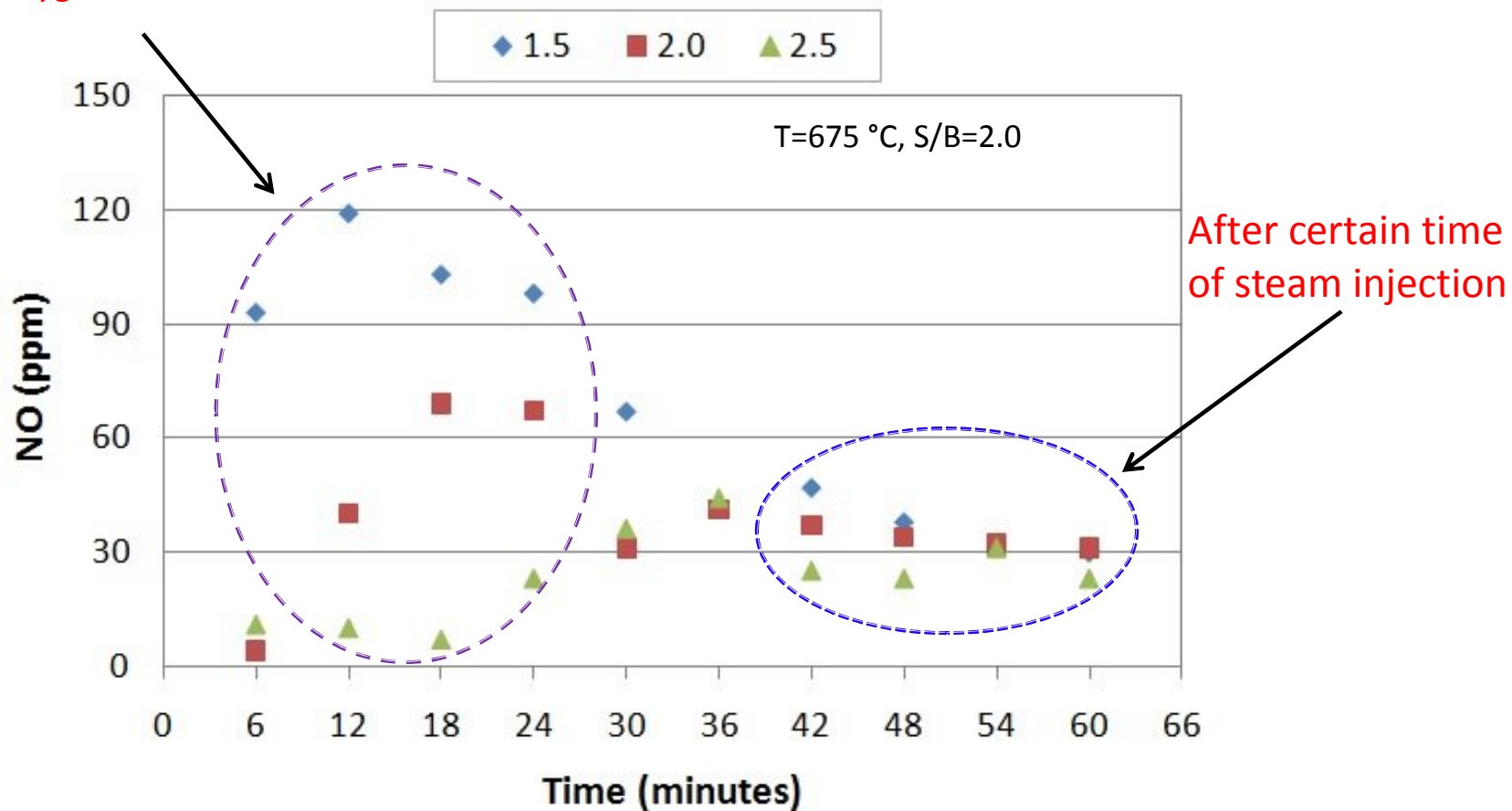
SO₂ Formation-Effect of Temperature



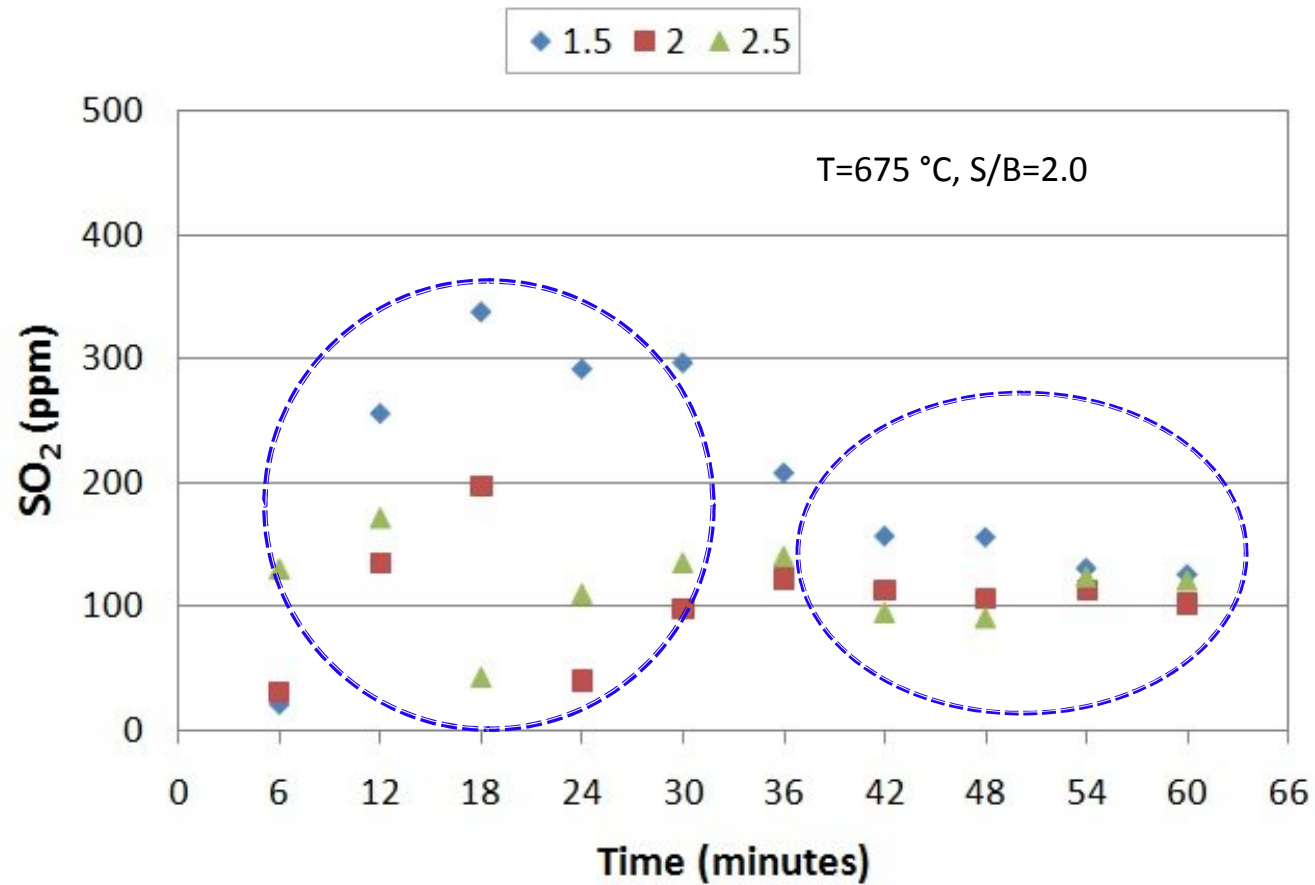


NO Formation-Effect of Steam to Biomass Ratio

High amount of steam produce oxygen deficient environment



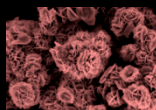
SO₂ Formation-Effect of Steam to Biomass Ratio

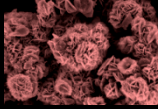


Comparative Study

Parameters	Current study	Sethuraman et al. (2010)	Ciferno et al. (2002)		Patel et al. (2001)
Reactor	FB ^a	FB ^a	FB ^a (MTCI) ^b	FB ^a (Sorfresid) ^c	FixB ^d
Biomass	Palm kernel shell	Wood	Pulp sludge	Municipal solid waste	Wood
Gasification agent	Steam	Air	Steam	Air	Steam
Temperature (°C)	675	815	790-815	1300-1400	843
Pressure (atm)	1.0	1	1	1	1
Steam/biomass	2.5	NA	-	-	-
Sorbent/biomass	1.0	1	-	-	-
Catalyst/biomass	0.1	NA	NA	NA	NA
N content (wt%)	1.02	0.14	-	2.3	3.75
S content (wt %)	0.27	-	-	0.3	0.64
NO (ppm)	30	215	25	120	477
SO ₂ (ppm)	110	NA	9 ^e	79 ^e	193

^aFluidized bed, ^b Manufacturing and technological conversion international, ^c Sorfresid/caliqua technologies, ^d Fixed bed, ^e SO_x.
 „..“ shows unknown or not reported^{NA} not applicable





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Acknowledgement



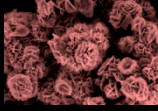
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Thank You