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pharmaceutics



A Novel Intensification Strategy for Wet Media Milling of Drug Suspensions: Bead Mixtures

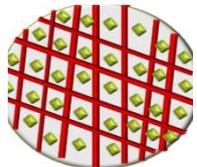
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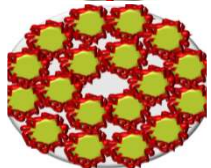
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Motivation

- Delivery of poorly water-soluble drugs remains a significant challenge (Kipp, 2004; Lipinski, 2002)
 - Up to 80-90% of drugs in pipeline are poorly water-soluble (Chawla and Bansal, 2007; Shah et al., 2006)
 - Require some form of bioavailability enhancement (Brough and Williams III, 2013)
- Available approaches to enhance the bioavailability:



– Amorphous solid dispersions (Forster et al. 2001; Hancock and Parks, 2000; Knopp et al. 2016)

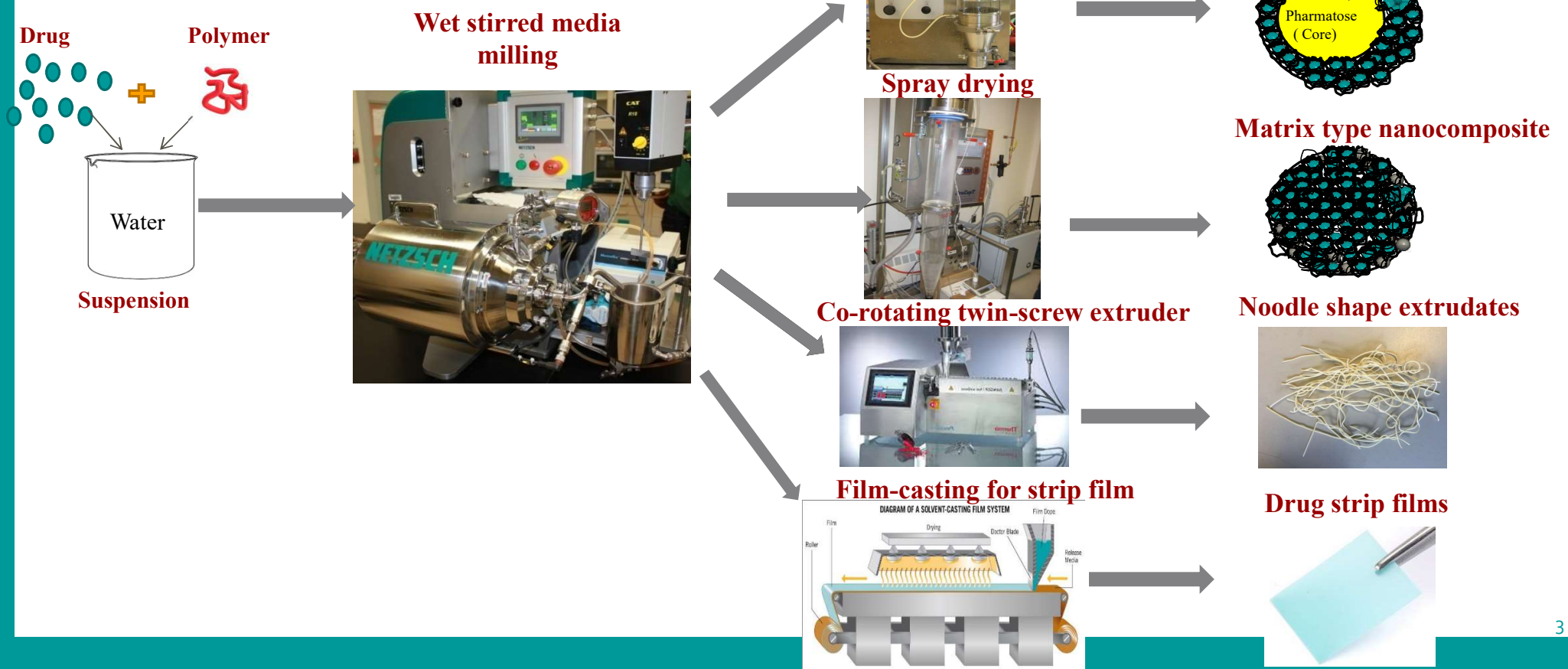


– Nanocomposites (Singh et al. 2011; Tanaka et al. 2012; Tuomela et al. 2014)

Noyes-Whitney equation

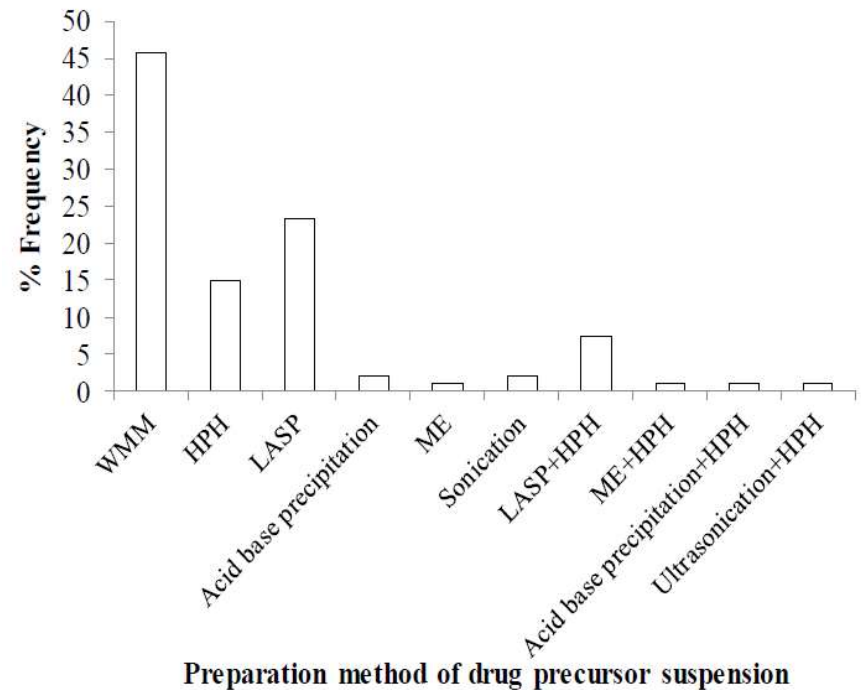
$$\frac{dm}{dt} = k_0 A (C_s - C)$$

Platform Approach: Nanocomposites Containing Drug Nanoparticles



Wet Stirred Media Milling

- **Advantages:**
 - Production of high drug-loaded, stable suspensions
 - Robust
 - Reproducible
 - Solvent-free
 - Environmentally benign
- **Disadvantages:**
 - Possible nanoparticle aggregation-growth
 - High energy consumption
 - Long operating hours
 - Contamination by the beads



Bhakay et al., (2018), *Pharmaceutics*, 10(3), 86.

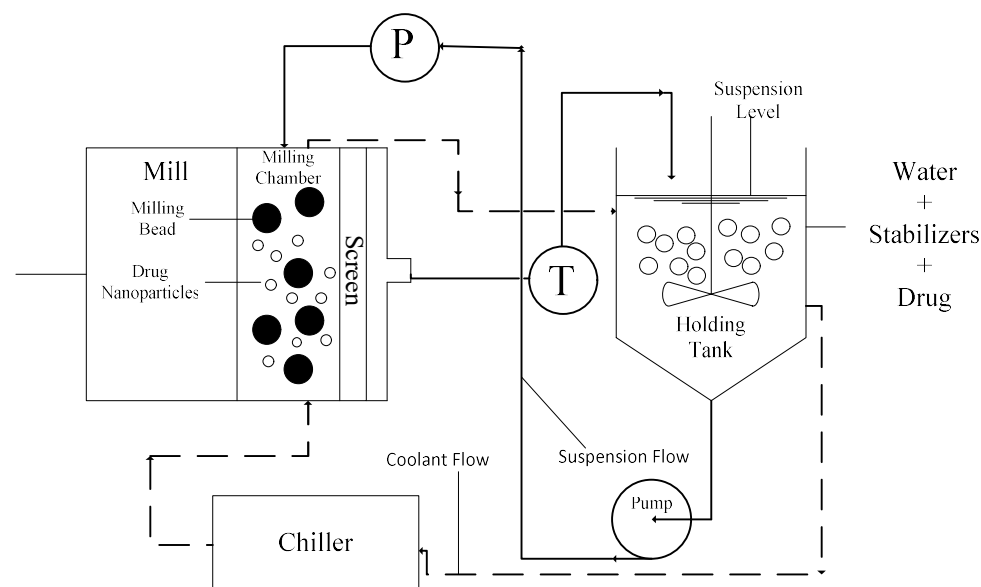
Wet Stirred Media Milling of Drugs

Purpose: Produce stable nanoparticle suspensions of BCS class II drugs

Mode of operation: Suspension is recirculated through the milling chamber

Mechanism of Action: Repetitive compression of drug particles captured between colliding beads (media)

Formulation: BCS class II drug and stabilizers (polymers and surfactants)



Previous Studies on Wet Stirred Media Milling: Process Optimization

- Afolabi et al. (2014) studied the impact of process parameters
- Li et al. (2017) studied the impact of Zirconia (YSZ) bead sizes and produced sub-100 nm nanoparticles (2015)
- Parker et al. (2020) studied the impact of crosslinked polystyrene (CPS) and YSZ beads
- A possible synergistic effect of CPS-YSZ bead mixture was not studied

	Polystyrene	Zirconia
ρ_b (kg/m ³)	1040	6000
Y_b (Gpa)	1.5 He et al., 2008	200 Ashby and Cebon, 1993
η_b	0.33 He et al., 2008	0.2 Srikar et al., 2004

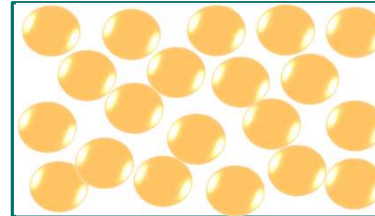
Experimental

- **Materials**

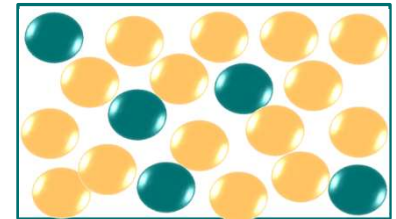
- Fenofibrate (drug): 10%
- Hydroxypropyl cellulose: 7.5%
- Sodium dodecyl sulfate: 0.05%
- 400 μm cross-linked polystyrene (**CPS**) beads and yttrium-stabilized zirconia (**YSZ**) (100:0-0:100)

- **Equipment**

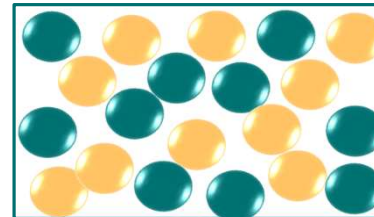
- Netzsch MicroCer wet stirred media mill
- Beckmann Coulter LS 230 for PSD
- Brookfield Rheometer



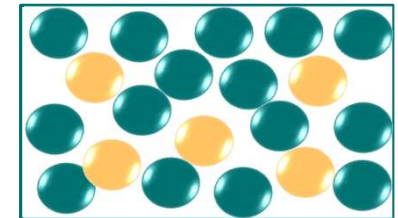
CPS:YSZ=100:0



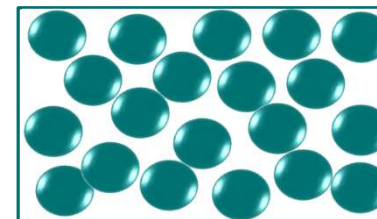
CPS:YSZ=75:25



CPS:YSZ=50:50

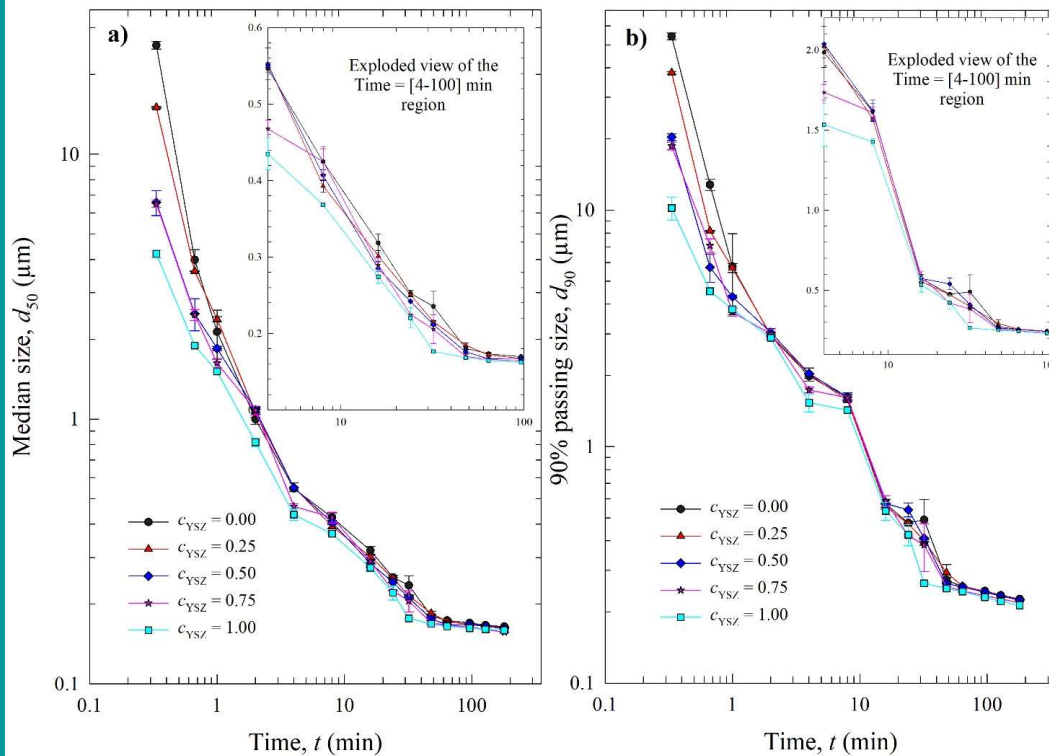


CPS:YSZ=25:75



CPS:YSZ=0:100

Wet Media Milling with Bead Mixtures



Initial drug particle size:

- $d_{50} = 25.58 \pm 0.06 \mu\text{m}$
- $d_{90} = 49.32 \pm 0.016 \mu\text{m}$

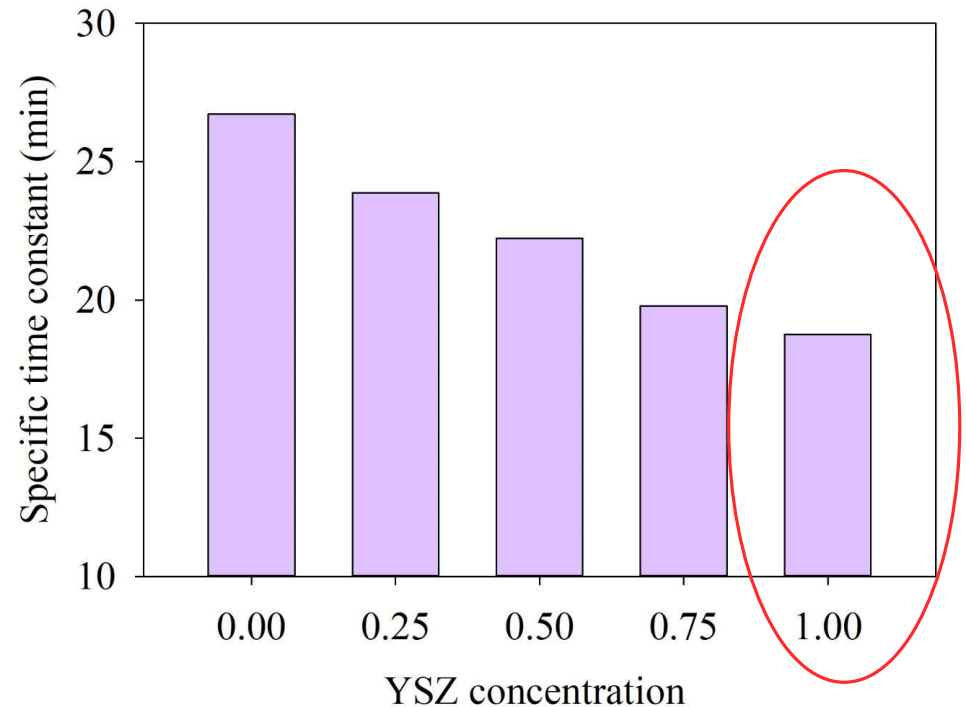
FNB nanosuspensions with $d_{50} < 165 \text{ nm}$ were produced within 180 min using CPS and YSZ beads and their mixtures

Well-stabilized suspensions: Monotonic decrease of particle size and no particle growth over 7 days (not shown for brevity)

Apparent grinding limit: $\sim d_{50} = 160 \text{ nm}$

Specific time constant

- Time required for d_{50} to reach $0.25\ \mu\text{m}$
- Faster breakage at higher YSZ concentration in the bead mixture
- The increase in the rate decreases for $\text{C}_{\text{YSZ}} > 0.5$

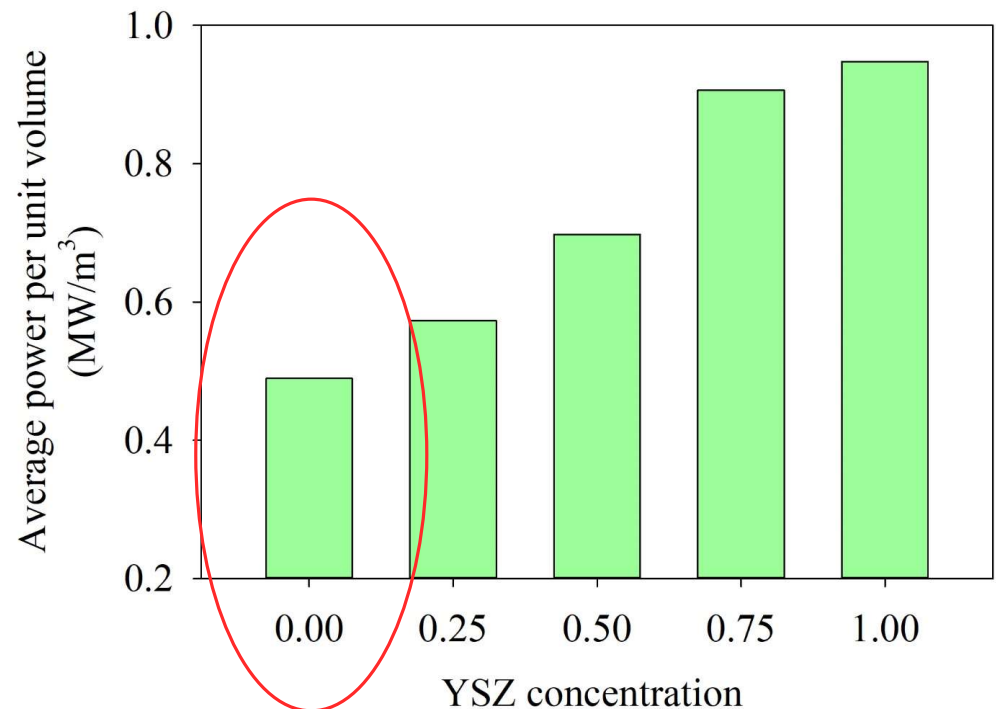


Power

- Power (P) was found by dividing the cumulative energy consumption read from the control panel of the mill by the milling time
- The average stirrer power per unit volume was found

$$P_w = \frac{P}{V}$$

- The more YSZ in the mixture, the more power required

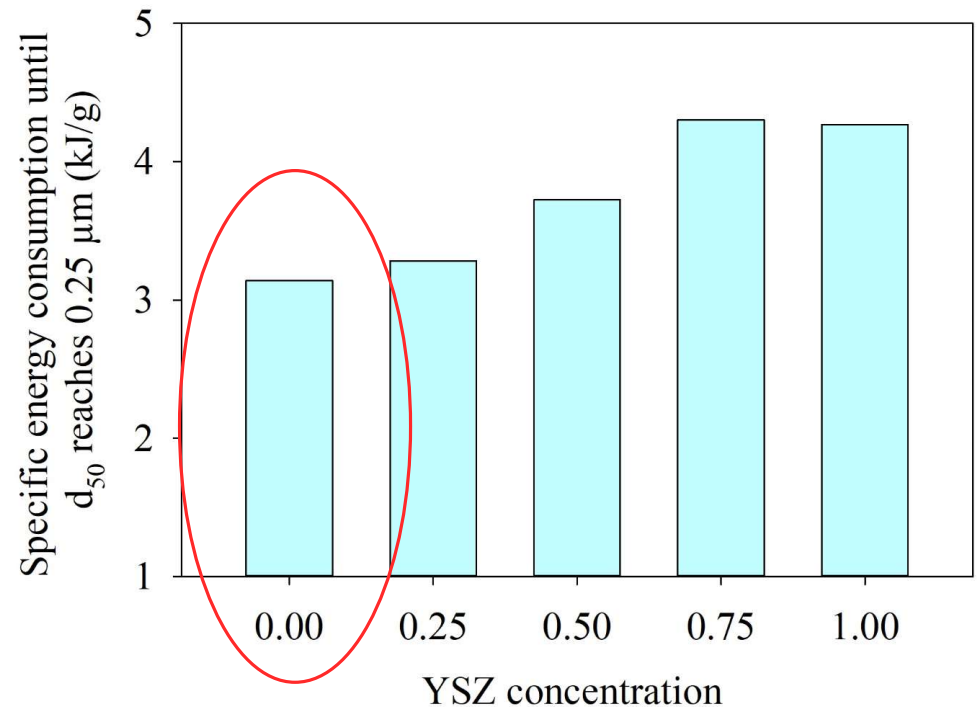


Energy consumption

- Specific energy consumption during d_{50} reaches $0.25 \mu\text{m}$ was found

- $$E_{td50} = \frac{P_w V_m t_{d50}}{m_D}$$

- Higher YSZ concentration caused higher energy consumption
- The increase in energy consumption was less pronounced than that in power.



Merit Score for an Optimum Process

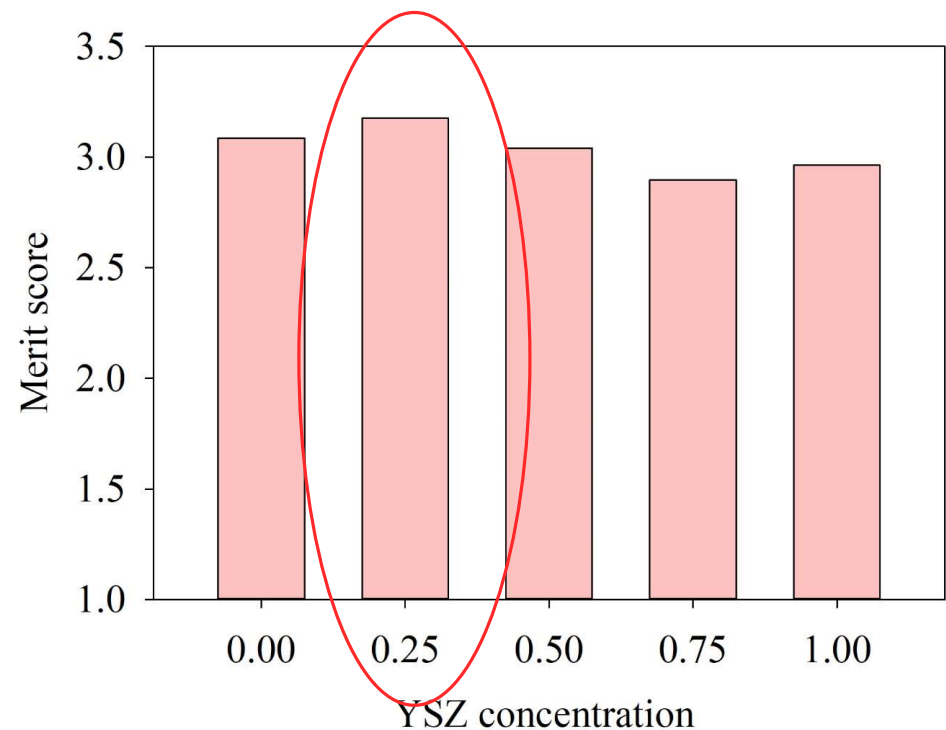
- Both breakage kinetics and energy consumption is considered

$$\bullet \overline{t_{d50}} = \frac{t_{d50}}{t_{d50,max} - t_{d50,min}}$$

$$\bullet \overline{E_{td50}} = \frac{E_{td50}}{E_{td50,max} - E_{td50,min}}$$

$$\bullet \textit{Merit score} = \frac{2}{\overline{t_{d50}} + \overline{E_{td50}}}$$

- Optimum was found in a mixture!



Conclusions

- CPS beads are favorable for energy efficiency (lower utility costs)
- YSZ beads are favorable for fast production (reduced cycle time)
- When the process is designed to reduce both, mixture of beads appears to enable optimization.
- Different operating conditions will be studied in future work.

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Thank you,
Any Questions?