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Development of aqueous two-phase systems based on deep eutectic solvents for continuous protein extraction in a microextractor

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Introduction

Due to growing tendency to develop processes that are more eco-friendly, the use of enzymes as catalysts is gaining more and more attention. Lipases are enzymes very often used in catalysis because they have a very wide specificity and maintain high activity in mild conditions. These trends require an efficient lipase purification so that its activity could be the highest possible. Conventional enzyme purification techniques are very expensive, time consuming, and, most importantly, complicated. Since proteins are basic components of lipase's structure, aqueous two-phase protein extraction is considered as a promising and flexible alternative purification method. Various solvents can be used as extraction mediums and so, in accordance with the principles of green chemistry, the use of biodegradable, non-toxic, and recyclable deep eutectic solvents (DESs) as protein extraction solvents is intensively investigated. Therefore, aqueous two-phase system (ATPSs) based on natural DES and its application for protein extraction in a microextractor, that ensures higher efficiencies due to microchannel geometry and a continuous process, were investigated in this research.

Results and Discussion

1 BATCH EXPERIMENTS

Table 1. Synthesized DESs and their properties







		DES	abbreviation	component molar ratio	water content, %	ρ, g/mL	pН	η (25°C), mPas	ν (25°C), mm²/s	80 - 60 - E, %
DES		cholin-chloride: urea	ChU	1:2	5	1.185	9.321	30.686	25.895	40 - 20 -
	25 °C	cholin-chloride: glycerol	ChGly	1:2	-	1.150	5.324	53.099	46.173	0 - ×
	30 min	cholin-chloride: ethylene glycol	ChEG	1:2	_	1.135	6.981	15.536	13.688	0.3 0.4
K ₂ HPO ₄		cholin-chloride: glucose	ChGlc	1:1	25	1.265	5.691	38.785	30.660	100
and		betain: glycerol	BGly	1:2	-	1.180	9.255	212.193	179.825	80 -
protein		betain: urea	BU	1:3	40	1.190	9.254	3.472	2.918	60 -
DES		$E = \frac{\gamma_{P,upper phase} \cdot V_{upper phase}}{\gamma_{P,upper phase} \cdot V_{upper phase} + \gamma_{P,bottom phase} \cdot V_{bottom phase}}$								20 - 0 - × ×
DES + proteins K ₂ HPO ₄ solution		Bradford protein assay				Optimal two-phase system features:				0.3 0.4
residual proteins		$\gamma_{P, upper phase} \gamma_{P, bottom phase}$				✓ DES BU ✓ $\gamma_{K_2HPO_4} = 0.7 \text{ g/mL}$				$80 - 60 - E_{\mu}\%$
E = 98.50%										$\begin{array}{c} 40 \\ 20 \\ 0 \\ \end{array}$





Conclusions

Aqueous two-phase systems based on six different natural DESs (Table 1.) for protein extraction were investigated. Optimal two-phase system features were determined through batch protein extraction experiments where the influence of salt concentration on protein extraction efficiency was monitored (Figure 1.). The highest efficiency of 94.70 % was achieved in ATPS based on DES BU with $\gamma_{K_2HPO_4} = 0.7 \text{ g/mL}$, so those conditions were declared optimal and used in further research. Protein extraction process was then transferred to a microextractor and carried out under optimal conditions at various retention times (Figure 2.). Highest extraction efficiency of 98.50 % was obtained for only 30 s which is an indication that the process was significantly intensified in comparison to batch experiments. Retention time of 30 s was therefore used in reusability experiments where DES was succesfully used in 7 cycles with efficiencies above 90 % (Figure 3.). Number of cycles could probably be even higher, but due to constant DES volume loss, additional cycles could not be conducted in this case. Finally, the developed extraction method was verified using raw lipase produced by Thermomyces *lanuginosus* solid-state cultivation on hull-less pumpkin oil pomace (Figure 4.) with somewhat lower efficiencies. However, considering that the highest protein extraction efficiency obtained with raw lipase sample was still relatively high (*E* = 85.04 % for retention time of only 12 s), this method can be considered as suitable for continuous



natural deep eutectic solvents, Sep. Purif. Technol., 244 (2020) 116746.