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## Model-Based Design and Optimization of Electrochemical Processes for Sustainable Aviation Fuels

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# Introduction : electrofuels for aviation

- 12% of the transport-related CO<sub>2</sub> emissions are from aviation
- 2-3% of all anthropogenic emission
- “Flight Path 2050”
  - a 75% reduction in CO<sub>2</sub> per passenger kilometer,
  - a 90% reduction in NO<sub>x</sub>
- For short range aviation : Electric aviation/battery/fuel cell system
- For long range : Electrofuels (Furfuryl alcohol, n-octane, ammonia, methane, hydrogen)

# Electroreduction of furfural

- The raw material, furfural is derived from hydrolysis of biomass
- No toxic catalyst/products, mild operating conditions
- Electrode materials studied: Graphite foil, Polycrystalline graphite sheet, Graphite felt, Lead sheet, Copper sheet, Copper gauze, Nickel sheet, Nickel gauze, Iron sheet, Aluminium sheet, and Platinum sheet
- Reactor types
- Reaction conditions

Mathematical model and systematic framework for process design and optimization missing in literature.

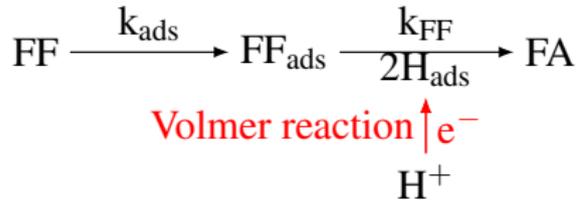
# Overview

- Part I : Simplified model for conversion of furfural to furfuryl alcohol
  - Model for furfural to furfuryl alcohol
  - Effect of overpotential on adsorbed hydrogen
  - Effect of overpotential on yield
- Part II : Extended model with conversion of furfural to furfuryl alcohol and methylfuran along with hydrogen evolution
  - Reaction scheme for model with adsorption, without adsorption and hybrid mechanism
  - Model for extended reaction scheme
  - Comparison of model prediction and experimental data

# Part I

## Simplified model for conversion of furfural to furfuryl alcohol

# Reaction scheme: furfuryl alcohol synthesis



- FF - Furfural
- $\text{FF}_{\text{ads}}$  - Adsorbed furfural
- $\text{H}_{\text{ads}}$  - Adsorbed hydrogen
- FA - Furfuryl alcohol

Red arrow: Electrochemical reaction,

Black arrow: Chemical reaction.

# Model assumptions

- The hydrogen fraction of adsorbed hydrogen remains the same during the reaction.
- There is no formation of additional byproducts such as methyl furan, methyltetrahydrofuran, and tetrahydrofurfuryl alcohol.
- The fraction of the surface area available for the reactions does not change over process time.
- Basic conditions.

# Model equations

Adsorption (furfural and hydrogen):

$$r_{\text{ads}} = k_{\text{ads}} \cdot \text{FF} \cdot \theta_{\text{v}},$$

$$\theta_{\text{H}_0} = \frac{1}{1 + \exp(-(p_1 + p_2 \cdot E))}.$$

Conversion of furfural to furfuryl alcohol

$$r_{\text{FF}} = k_{\text{FF}} \cdot \theta_{\text{H}}^2 \cdot \text{FF}_{\text{ads}}.$$

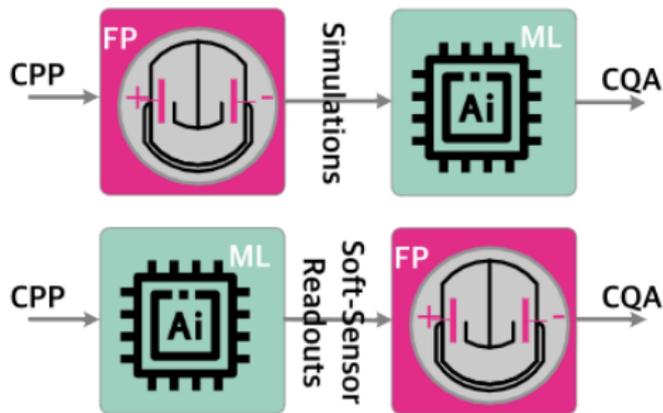
Material balance equations:

$$\frac{d\text{FF}_{\text{ads}}}{dt} = C(r_{\text{ads}} - r_{\text{FF}}),$$

$$\frac{d\text{FF}}{dt} = \frac{Q_{\text{in}}}{V} \text{FF}_{\text{in}} - r_{\text{ads}} a - \frac{Q_{\text{out}}}{V} \text{FF},$$

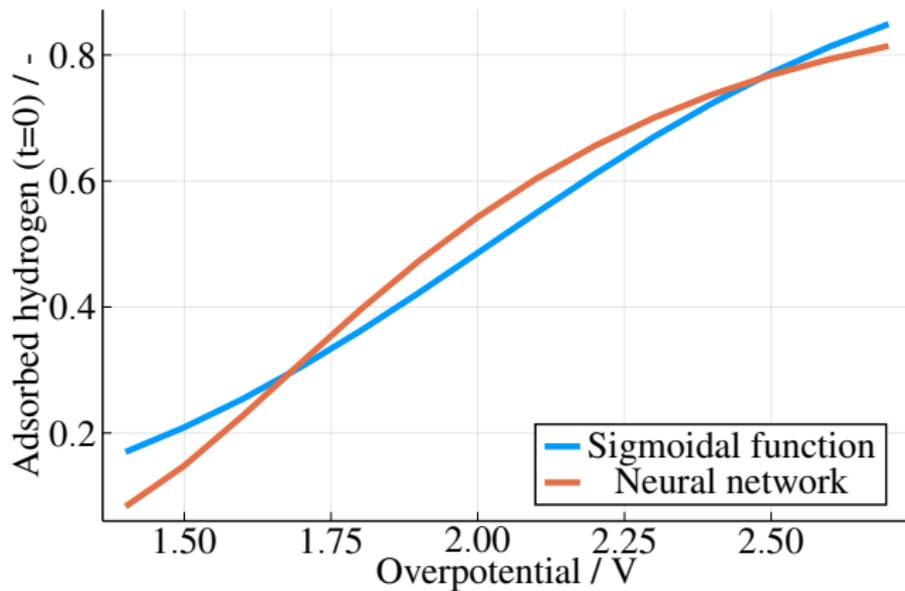
$$\frac{d\text{FA}}{dt} = \frac{Q_{\text{in}}}{V} \text{FA}_{\text{in}} + r_{\text{FF}} a - \frac{Q_{\text{out}}}{V} \text{FA}.$$

# Model overview

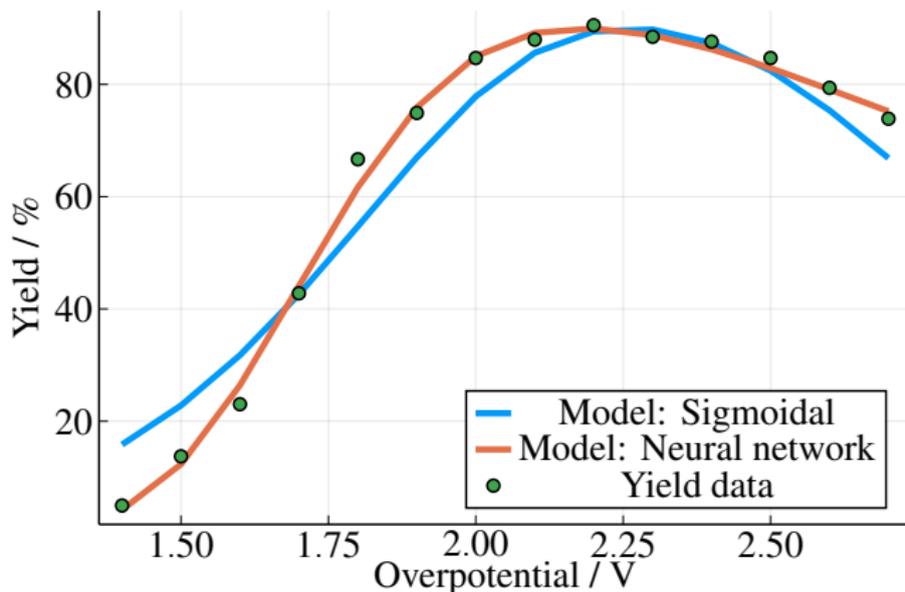


- Initial conditions : Furfural, furfuryl alcohol and adsorbed hydrogen (sigmoid function/Neural Network)
- Reaction dynamics: ODEs

# Effect of overpotential on adsorbed hydrogen



# Effect of overpotential on yield (ML + process model)



Furfuryl yield data from literature<sup>1</sup>  
<sup>1</sup> (Cao2019)

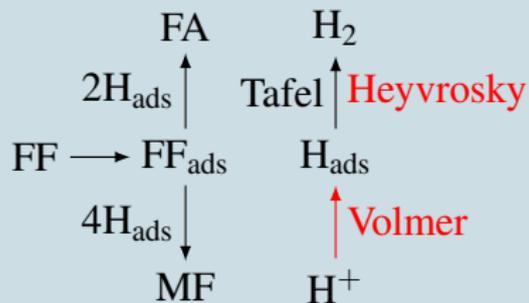
## Part II

# Extended model with conversion of furfural to furfuryl alcohol and methylfuran along with hydrogen evolution

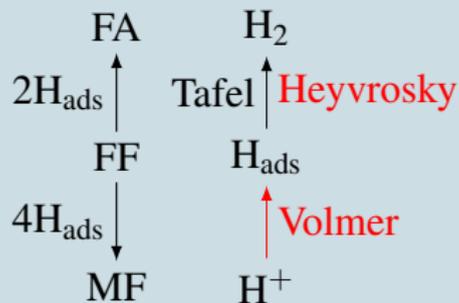
Acknowledgement: Dr.-Ing. Fabian Kubanek (InES) and Thorben Lenk (IÖNC)

# Reaction scheme: Furfuryl Alcohol (FA), Methyl Furan (MF) and H<sub>2</sub>

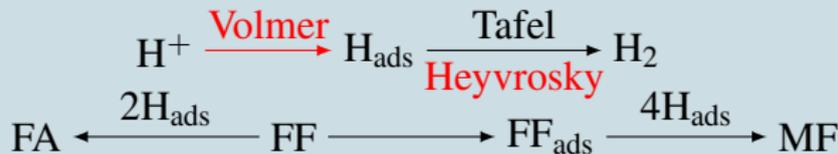
## Case 1: With adsorption



## Case 2: Without adsorption



## Case 3: Hybrid mechanism



# Model assumptions

- The formation of adsorbed hydrogen by Volmer reaction and adsorption of furfural on the electrode surface are reversible reactions and follows Frumkin type isotherm
- The conversion of furfural to furfuryl alcohol and methylfuran are irreversible reactions
- Evaporative loss of furfuryl alcohol and methyl furan

# Model equations

- Case 1:

$$r_{FA} = k_{FA} \cdot FF_{ads} \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot FF_{ads} \cdot H_{ads}^2$$

- Case 2:

$$FF_{ads} = 0 \text{ \& } \theta_{FF} = 0$$

$$r_{FA} = k_{FA} \cdot FF \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot FF \cdot H_{ads}^2$$

- Case 3:

$$r_{FA} = k_{FA} \cdot FF \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot FF_{ads} \cdot H_{ads}^2$$

$$\frac{d\theta_H}{dt} = \frac{F}{\sigma} [r_v - r_T - r_H - r_{FA} - r_{MF}]$$

$$\frac{d\theta_{FF}}{dt} = \frac{F}{\sigma} [r_{FFads} - r_{FA} - r_{MF}]$$

$$\frac{dFF}{dt} = -r_{FFads} \cdot a$$

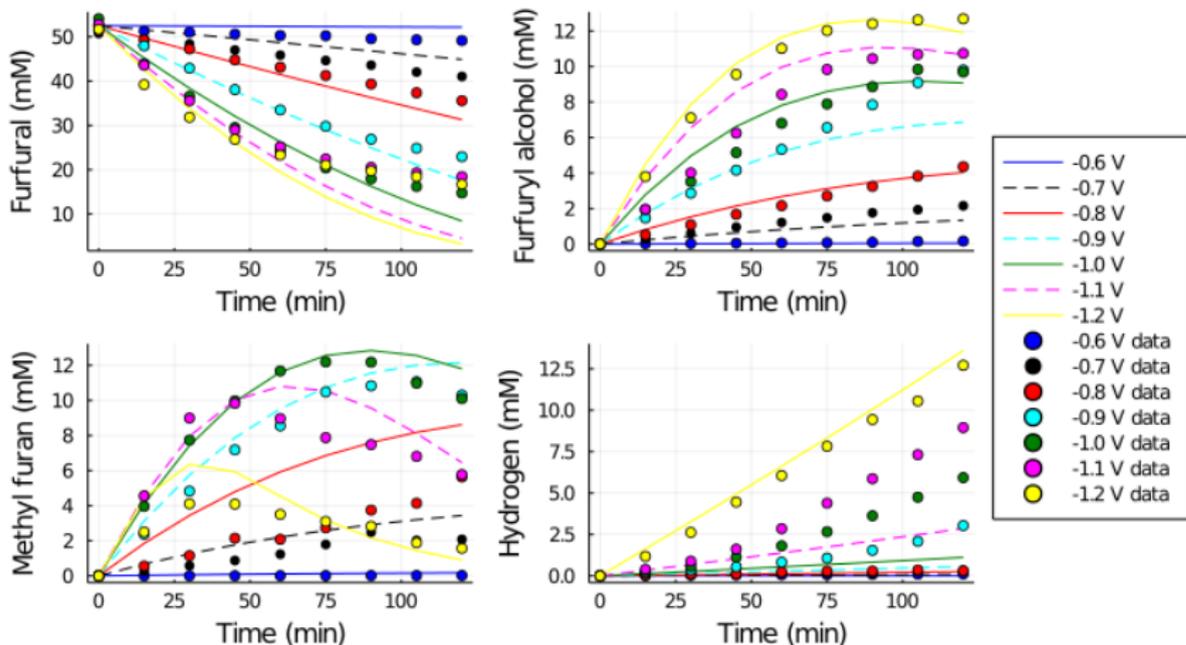
$$\frac{dFF_{ads}}{dt} = r_{FFads} - r_{FA} - r_{MF}$$

$$\frac{dFA}{dt} = r_{FA} \cdot a - r_{evap,FA}$$

$$\frac{dMF}{dt} = r_{MF} \cdot a - r_{evap,MF}$$

$$\frac{dH_2}{dt} = (r_T + r_H) a$$

# Results: Hybrid mechanism



# Summary and conclusions

- The concept of hybrid modeling implemented for a simplified model for electroreduction of furfural for overpotential between 1.4 to 2.7 V.

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Feature Paper

Article

## Hybrid Process Models in Electrochemical Syntheses under Deep Uncertainty

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- The extended model with hybrid mechanism fits the experimental data better. The model structure developed can be used for further studies on model-based optimization.



SE<sup>2</sup>A

Cluster of Excellence “SE<sup>2</sup>A - Sustainable and Energy-Efficient Aviation”, TU Braunschweig.

Thank You!

# Model parameters for simplified model

Table 1: Model parameters and initial value for electrochemical synthesis of furfuryl alcohol.

Parameter	$k_{\text{ads}}$	$k_{\text{FF}}$	C	FF( $t = 0$ )	FA( $t = 0$ )
Value	0.5969	$5.6437 \times 10^{-8}$	$1.6081 \times 10^9$	$0.1 \times 10^{-3}$	0
Unit	$\text{cm s}^{-1}$	$\text{s}^{-1}$	-	$\text{mol cm}^{-3}$	$\text{mol cm}^{-3}$

# Rate equations - case 1

$$r_v = k_{f,v} \theta_v \exp(-\lambda \cdot u_{f,h} \cdot \theta_H) - k_{b,v} \theta_H \exp((1 - \lambda) \cdot u_{b,h} \cdot \theta_H)$$

$$k_{f,v} = k_{f,v}^0 \exp(-\beta \cdot f \cdot E_c)$$

$$k_{b,v} = k_{b,v}^0 \exp((1 - \beta) \cdot f \cdot E_c)$$

$$r_{FFads} = r_{FFadsf} - r_{FFadsb}$$

$$r_{FA} = k_{FA} \cdot F_{ads} \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot F_{ads} \cdot H_{ads}^2$$

$$r_T = k_T \cdot \theta_H^2$$

$$r_H = k_H \cdot \theta_H$$

$$k_H = k_H^0 \cdot \exp(-\beta f E_c)$$

$$r_{HER} = (r_T + r_H) \cdot a$$

# Adsorption and evaporation kinetics

$$r_{FFadsf} = k_{f,ads} \cdot FF \cdot \theta_v \cdot \exp(-\lambda \cdot u_{f,f} \cdot \theta_{FF})$$

$$r_{FFadsb} = k_{b,ads} \cdot \theta_{FF} \cdot \exp((1 - \lambda) \cdot u_{b,f} \cdot \theta_{FF})$$

$$r_{evap,MF} = (k_{evap,MF,1} \cdot H_2 + k_{evap,MF,2}) \cdot MF$$

$$r_{evap,FA} = (k_{evap,FA,1} \cdot H_2 + k_{evap,FA,2}) \cdot FA$$

# Rate equations - case 2 & 3

Case 2:

$$r_{FA} = k_{FA} \cdot FF \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot FF \cdot H_{ads}^2$$

Case 3:

$$r_{FA} = k_{FA} \cdot FF \cdot H_{ads}^2$$

$$r_{MF} = k_{MF} \cdot F_{ads} \cdot H_{ads}^2$$