

RSM Process Optimization of Biodiesel Production from Waste Cooking Palm Oil in the Presence of SO₃H-PSC Catalyst †

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Abstract: This research studied about the synthesis of green and novel catalyst from waste materials for biodiesel production. An activated carbon (AC) material from palm seed cake (PSC) was soaked with zine chloride (ZnCl₂) and treated with sulfonic acid (SO₃H). The use of a sulfonated palm seed cake (SO₃H-PSC) derived catalyst for the transesterification/esterification of triglyceride (TG) in waste cooking palm oil (WCPO) has been demonstrated. The synthesized SO₃H-PSC catalyst was characterized using powder X-ray diffraction (XRD), Fourier transform infrared spectrometer (FTIR), scanning electron microscopy (SEM), energy dispersive spectrometer (EDS) and Brunauer-Emmet-Teller (BET) method. To study the effects of methanol/oil mole ratio, amount of catalyst, and reaction time, the process of biodiesel production in a microwave reactor was optimized using a Box-Behnken design (BBD) approach with response surface methodology (RSM). As a result, the optimum reaction parameters found were 5.40 wt.% of the SO₃H-PSC catalyst, 17.35:1 methanol/WCPO mole ratio, and 8.57 min of reaction time. The synthesized biodiesel from WCPO meets the criteria for standard biodiesel (ASTM D-6751 and EN 14214). The heterogeneous catalyst demonstrates a promising and effective application for biodiesel process especially for feedstocks containing high free fatty acid (FFA) content.

Keywords: activated carbon; palm seed cake; heterogeneous catalyst; waste cooking palm oil; biodiesel process; optimization; Box-Behnken design; response surface methodology

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1. Introduction

Due to population growth and accelerated industrial development, the demand for fossil fuels has increased despite their negative environmental impact. This situation has prompted the search for environmentally friendly and sustainable alternative energy sources [1]. Recently, biodiesel has become more popular due to its environmental benefits and the fact that it is derived from renewable resources. The transesterification/esterification of triglyceride (TG) in vegetable oils with methanol (CH₃OH) or ethanol (C₂H₅OH), as well as the principal applications of the fatty acid methyl esters (FAMES) or fatty acid ethyl esters (FAEEs), are discussed in the body of work [2,3]. The procedure can be catalyzed chemically or enzymatically, and it can also be performed under supercritical circumstances without the use of a catalyst. The typical catalysts for this method are consistent strong bases or acids. Because of environmental constraints and process simplifications, homogeneous catalysts are going to be mostly substituted by heterogeneous catalysts in the near future [4].

A variety of substrates have been used to prepare heterogeneous catalysts for biofuel synthesis. However, many noted drawbacks to using these catalysts, including higher biofuel production costs, intensive reaction conditions, and poor reusability. Alternatively, in

recent years, biomass-based support material has acquired popularity due to its cheap cost and minimal environmental impact during heterogeneous catalyst production. Here, carbon derived from biomass, also known as activated carbon (AC), has acquired popularity due to its many desirable physiochemical properties, wide supply, and low cost [5]. Because of their chemical inertness and excellent mechanical and thermal stability, carbon-based solid acids are viewed as perfect catalysts for many reactions. Carbon structures, whether aromatic or cyclic, abundant in the oxygenated functional group are thought to be present in the solid catalyst produced from material with high levels of lignin and carbohydrates [6].

Palm oil is derived from the fruit of the oil-palm tree. Oil palm mills produce a significant amount of both liquid and solid waste. Given the significant quantities of solid waste generated by oil palm mills, there is a need for their recovery and/or recycling. These wastes are presently either disposed of in landfills or burned for energy production [7]. The goal of this study was to develop a method for making a solid acid catalyst from organic refuse products commonly found in Thailand factories, especially palm seed cake (PSC). To enhance working factors, the response surface method (RSM) is applied. It is used to assess many components and their interactions, as well as to reduce the number of required experimental trials in order to speed up and correctly carry out the experimental process. The Box-Behnken design (BBD) is one of many available designs at RSM that have been widely used to improve biodiesel process. This is because BBD can predict, is more effective at parameter tuning, and requires fewer trials than other systems.

2. Materials and Methods

The PSC was gained from Absolute Palm Co., Ltd., Thailand. The waste cooking palm oil (WCPO) feedstock containing high free fatty acid (FFA) content was obtained for free from a number of restaurants in the surrounding area of Silpakorn University in Nakhon Pathom, Thailand. It was first filtered to eliminate impurities before being heated in an oven at 100 °C for 30 min to remove any residual wetness. Zinc chloride ($ZnCl_2$), sulfonic acid (SO_3H) and methanol were analytical grade chemicals (Merck Ltd., Thailand, greater than 99% purity) that were used precisely as received.

In brief, after pyrolysis of soaked PSC with $ZnCl_2$, the PSC-based acidic catalyst was developed via a sulfonation process. The previous method [8] for preparing the sulfonated palm seed cake (SO_3H -PSC) derived catalyst was followed and slightly modified. Powder X-ray diffraction (XRD), Fourier transform infrared spectroscopy (FTIR), scanning electron microscopy (SEM), energy dispersive spectroscopy (EDS), and the Brunauer-Emmet-Teller (BET) technique were used to characterize the novel catalyst.

By applying BBD of RSM, the effect of reaction parameters such as catalyst quantity (3–7 wt.%), methanol/WCPO mole ratio (12–18), and reaction time (5–9 min) on %yield of FAME (biodiesel) was examined. Each test was performed 3 times, and the standard deviation at any given point never exceeded 7%. A quadratic polynomial equation was generated utilizing Design-Expert® Software, version 13 (Stat-Ease, Inc., Minneapolis, MN, USA). The analysis of variance (ANOVA) test was employed to evaluate the model's fit [9]. Using gas chromatography-mass spectrometry (GC-MS), the biodiesel's composition was identified. The catalyst quantity (A), methanol/WCPO mole ratio (B), and reaction time (C) were the three independent factors in a three-variable BBD that was optimized through 15 experiments. Table 1 displays the three independent variables' actual amounts in coded values. Figure 1 depicts the RSM process for producing biodiesel using SO_3H -PSC catalyst from WCPO and methanol in a microwave reactor.

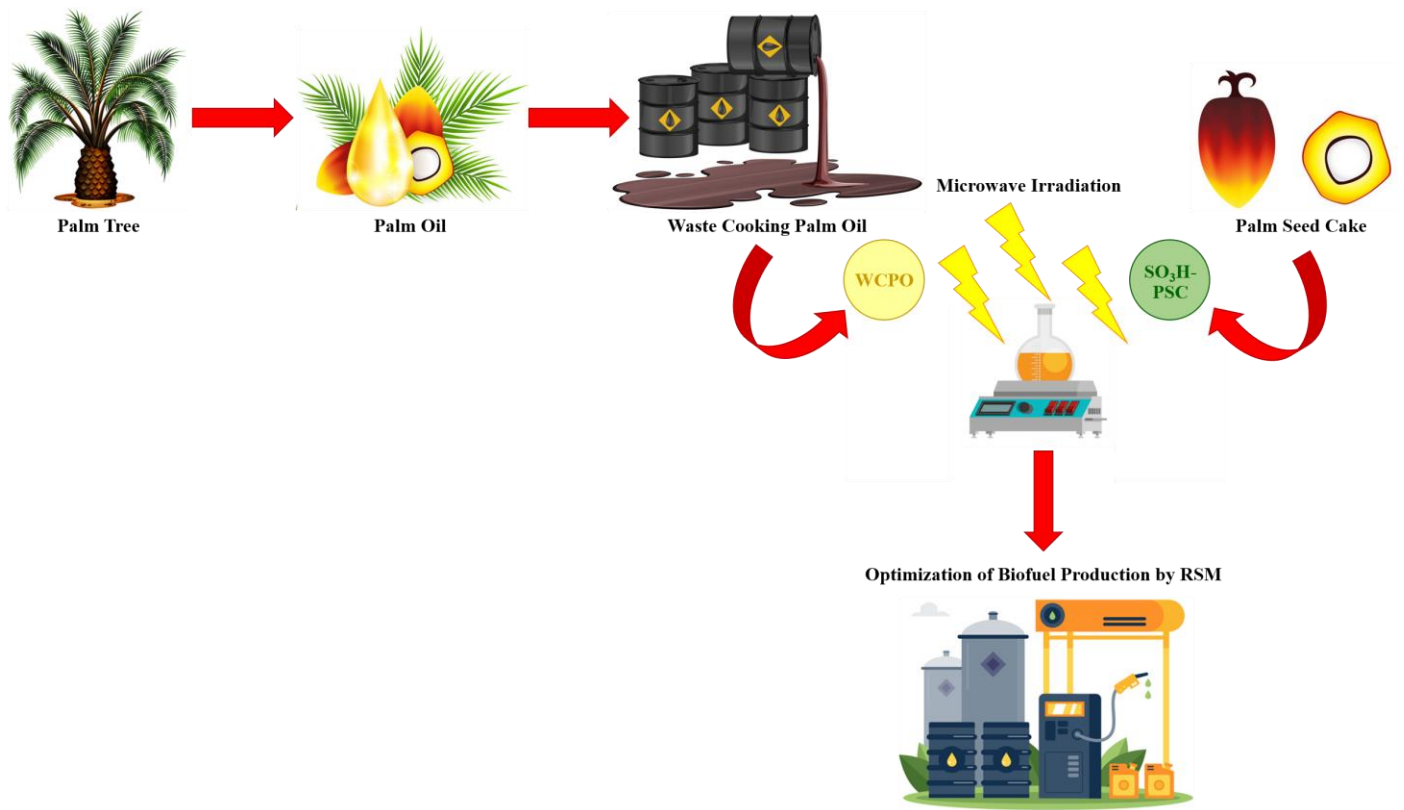


Figure 1. Scheme of the production of biodiesel from WCPO and methanol using $\text{SO}_3\text{H-PSC}$ catalyst with a microwave reactor.

Table 1. Factors and levels of RSM process for biodiesel production.

| Factors | Levels | | |
|---------------------------------------|--------|----|----|
| | -1 | 0 | +1 |
| Catalyst quantity (A), wt.% | 3 | 5 | 7 |
| Methanol/WCPO mole ratio (B), mol/mol | 12 | 15 | 18 |
| Reaction time (C), min | 5 | 7 | 9 |

3. Results and Discussion

Figure 2 depicts the XRD patterns of the PSC and $\text{SO}_3\text{H-PSC}$ catalyst. The samples showed one broad and one weak peak at $2\theta = 10^\circ\text{--}30^\circ$ and $2\theta = 40^\circ\text{--}50^\circ$, corresponding to C (0 0 2) and C (1 0 1), respectively. The broad peaks around $2\theta = 10^\circ\text{--}30^\circ$ are a typical feature of amorphous carbon, which includes aromatic carbon sheets. Meanwhile, the sharp peak is ascribed to graphite’s crystalline 3-dimensional region [6].

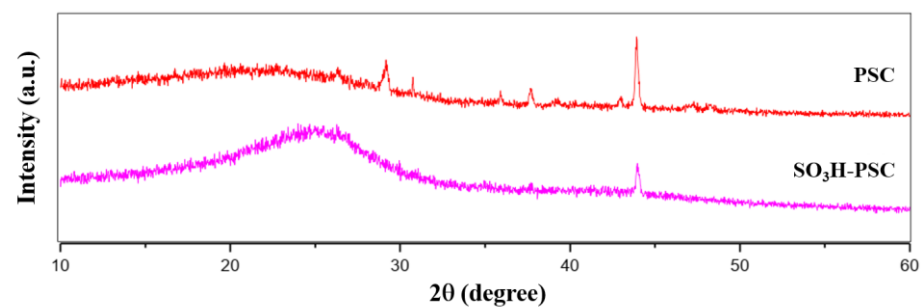


Figure 2. XRD patterns of PSC and $\text{SO}_3\text{H-PSC}$ samples.

The FTIR spectra of the PSC and SO₃H-PSC samples are displayed in Figure 3. The FTIR transmission at 1195 cm⁻¹ for –SO₂ asymmetric stretching and 1050 cm⁻¹ for –SO₂ symmetric stretching can detect the presence of sulfonic groups (–SO₃H). Rashid et al. [5] reported almost identical outcomes for a sulfonated carbon catalyst derived from residual carbohydrates.

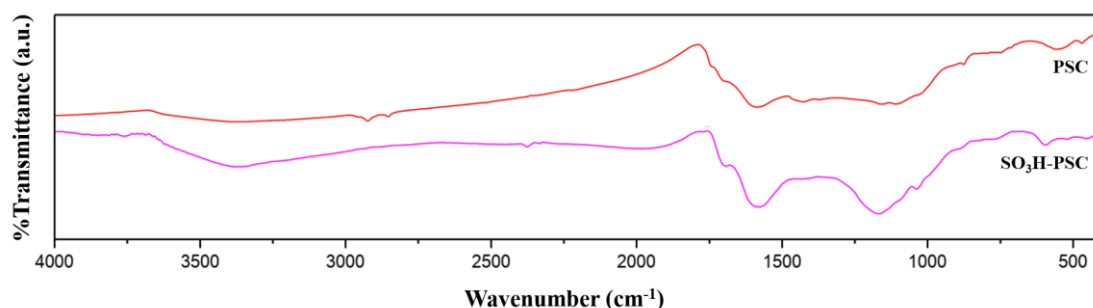


Figure 3. FTIR spectra of PSC and SO₃H-PSC samples.

Figure 4 represents the SEM image of a sample of SO₃H-PSC. The particles of the catalyst were agglomerated and irregular. After soaking in ZnCl₂ and sulfonation with SO₃H, the surface texture of the raw material was drastically altered [8]. Furthermore, Figure 4 shows the EDS spectrum and the elemental composition of the SO₃H-PSC catalyst. With atomic percent values of 64.49, 32.95, and 2.56, respectively, carbon (C), oxygen (O), and sulfur (S) were evidently the primary components of the solid catalyst. During the modification process, the acid content would be deposited on the catalyst's surface as opposed to the catalyst pores.

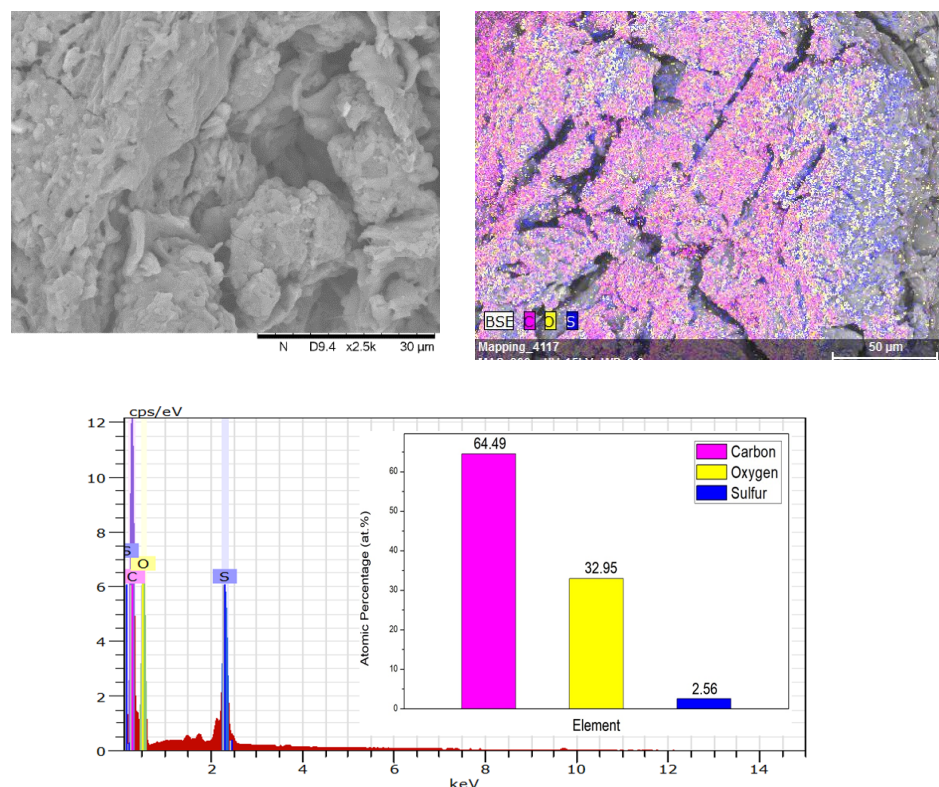


Figure 4. SEM image and EDS analysis of SO₃H-PSC sample.

The SO₃H-PSC catalyst had a pore volume of 0.32 cm³/g and a BET surface area of 14.83 m²/g. The substantial decrease in the BET surface area of the catalyst indicates that

acid molecules (SO₃H groups) have occupied the AC's pores, supporting the previously stated concept [10]. Furthermore, it is evident that the catalyst substantially increased the number of active sites.

They found that increasing the reaction time from 5 to 9 min at the methanol/WCPO mole ratios of 12:1 to 18:1 resulted in a higher percentage output of biodiesel (FAME). Furthermore, when the catalyst quantity exceeds the optimal value of 5 wt.%, the percentage of biodiesel yield decreases [11]. The contour plots in Figure 5 are the excellent visual representation of this study. The cubical representation of the parameters demonstrates how each parameter affects the biodiesel output in percentage terms. Analyzing the order in which these factors appear also aids [12]. The optimal operating parameters for achieving 98.92% biodiesel yield are a catalyst quantity of 5.40 wt.%, a methanol/WCPO mole ratio of 17.35:1, and a reaction time of 8.57 min. According to the GC-MS characterization report, WCPO is a great feedstock for the manufacturing of biofuel.

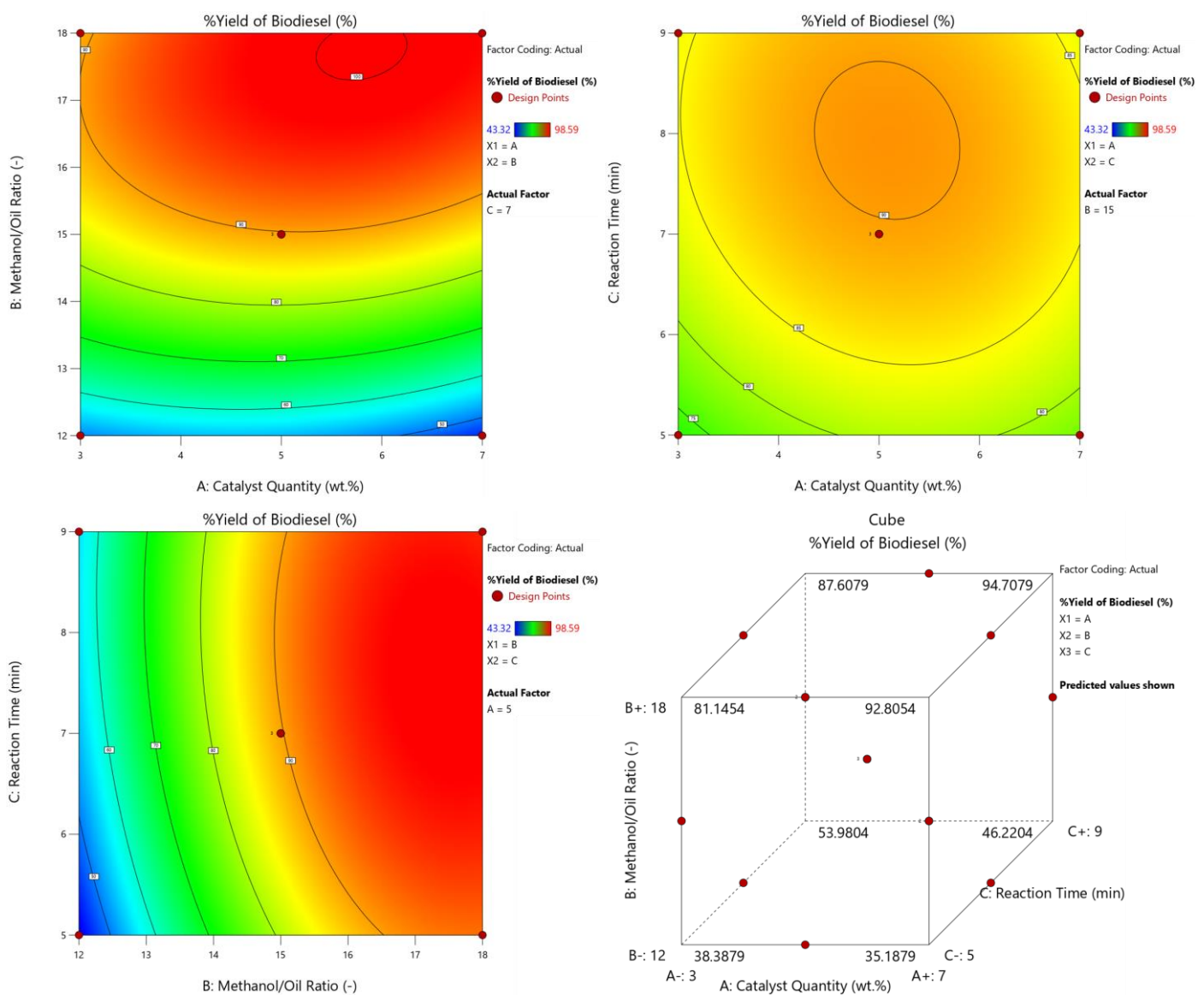


Figure 5. Optimal reaction conditions by contour plots of the catalyst quantity, methanol/oil ratio and reaction time, and cubical representation of effects of various parameters on %yield of biodiesel.

The fuel properties of biodiesel obtained in this study, such as kinematic viscosity, density, flash point, cloud point, pour point, acid value, and moisture content, satisfy the requirements for standard biodiesel (ASTM D-6751 and EN 14214). The majority of its properties fall within the range of fuel properties specified in the most recent biodiesel standards [13].

4. Conclusions

In this investigation, the synthesis of a SO_3H -PSC catalyst for biodiesel production has been demonstrated. The novel catalyst was successfully applied to highly acidic WCPO, which yielded approximately 98% biodiesel. RSM algorithm was utilized to validate the optimal yield outcomes.

Supplementary Materials: The following supporting information can be downloaded at: www.mdpi.com/xxx/s1.

Author Contributions: The present work was produced through a collaborative effort involving all of the authors. A.B. was responsible for the conceptualization of the experiments, data analysis, and the initial drafting of the manuscript, which was subsequently revised thoroughly. The experiments in the laboratory were conducted by P.S., S.P., and O.B.; V.L. made contributions to the conceptual approach and results discussion, and provided approval for the final version of the revised manuscript. All authors have read and agreed to the published version of the manuscript.

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