

# The 3rd International Electronic **Conference on Catalysis Sciences**

23-25 April 2025 | Online

## Degradation of endocrine disruptors via photocatalysis in a continuous-flow microreactor: a proposal for numbering-up

Nelda Xanath Martinez-Galero 1, Miguel Angel García-Muñoz 1 Adolfo Amador-Mendoza 2 Rocío Meza-Gordillo 3 Sebastián López-Martínez 4 1 Instituto de Química Aplicada del Centro de Investigaciones Científicas Universidad del Papaloapan; 2 Instituto de Agroingeniería Universidad del Papaloapan; 3 Instituto Tecnológico de Tuxtla Gutiérrez TecNM; 4 Ingeniería en Biotecnología Universidad del Papaloapan

0.9

0.8

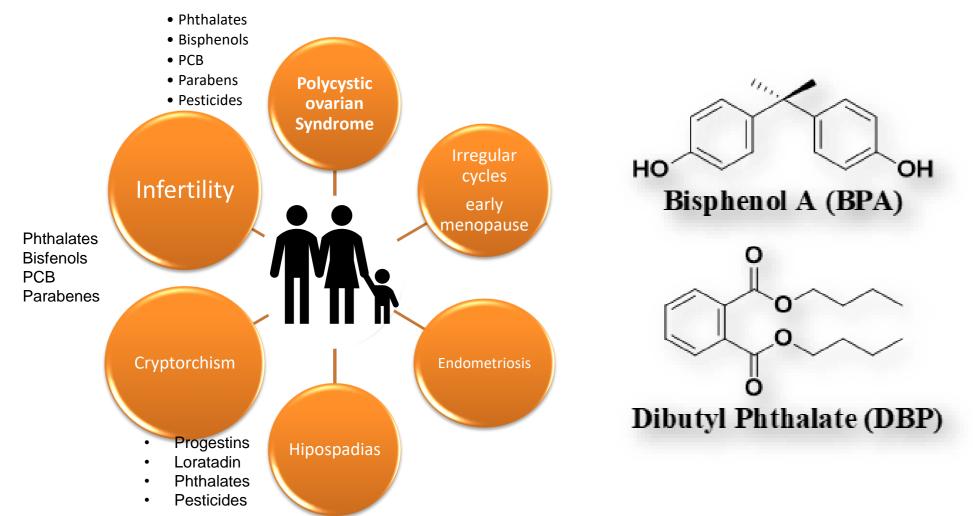
0.7

**EBPAt/BPA0** 

0.2

### **INTRODUCTION & AIM**

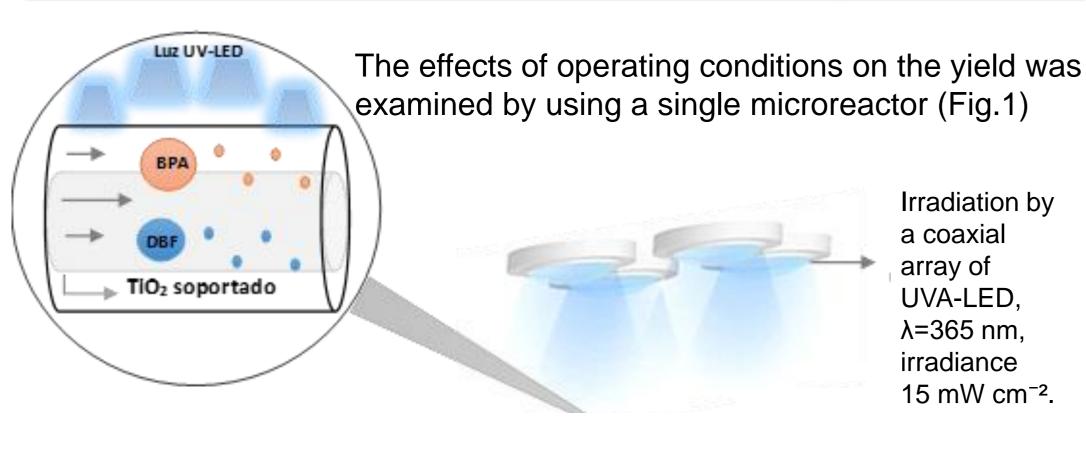
**Endocrine disrupting chemicals (EDCs) are exogenous** agents involves with the human and animal reproductive health [1].



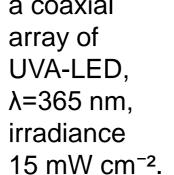
#### **RESULTS & DISCUSSION Reaction Order** ln [BPAt/BPAo] = 13.471t+ 0.3131 **BPA Reaction Kinetics** $R^2 = 0.9887$ Exp $R^2 = 0.9983$ Exp 6 Exp 14 Exp 16 pH = 4, T = 20 °C, Q = 1.0 mL/min, H<sub>2</sub>O<sub>2</sub> = 0 ppm Logarítmica (Exp 2) $R^2 = 0.996$ Logarítmica (Exp 6) ... • ... Experiment 6 pH = 4, T = 40 °C, Q = 1.0 mL/min, H2O2 = 2 ppm Lineal (Exp 14) •••• Experiment 14 pH = 10, T = 40 °C, Q = 1.0 mL/min, H2O2 = 2 ppm ••••••• Experiment 16 pH = 10, T = 40 °C, Q = 10.0 mL/min, H2O2 = 2 ppm $R^2 = 0.9899$

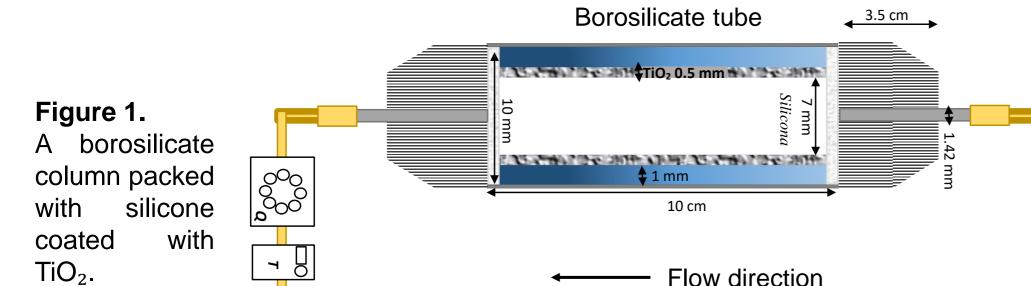
In this work, the efficiency of a continuous-flow photo-microreactor with TiO2 supported and irradiated by UVA-LED was evaluated, considering the effects of its operating conditions on the degradation of two endocrine disruptors, BPA and DBP.

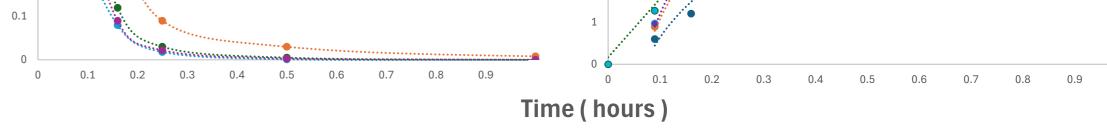
### METHOD











Graphic 1. The photodegradation rate of BPA and DBP by this UV/TiO2/µreactor process to obey pseudo first-order kinetics represented by the Langmuir-Hinshelwood model.

Table 2. Response variables											
	DE	C0 (µM)	<b>Control Variables</b>					<b>Response Variables</b>			
			t (h)	pН	Т (°С)	Q (mL/min)	[H <sub>2</sub> O <sub>2</sub> ] ppm	ERD %	$\frac{\mathbf{k}_{app}}{(\mathbf{min}^{-1})}$	$\mathbb{R}^2$	t <sub>1/2</sub> (min)
	BPA	438.3	0.25 0.25	10 4	40 40	1.0 1.0	2 2	99.2 97.5	0.2397 0.1974	0.9957 0.9960	5.4 7.7
	DBP	35.9	0.25	4 4	40 40	1.0 1.0	2 2	62.3 87.1	0.0639	0.9867	12.0

A proposal for numbering-up

With these results, an array four

borosilicate columns in parallel to

degrade BPA (Figure 2, only two of

them), using Exp 14's control variables

and considering that the viscosity is

less than 100 cP. The following were

required: mixer, flow splitter, and

needle valves (1/8") controlled by a

timer. Thus, a DRE was obtained at the

process outlet (93%).

## **Cleaner Water** Peltier controls flow control valve Piston pumps mixer / splitter box **Contaminated Water**

MDPI

**Table 1.** DoE 2<sup>4</sup> was implemented to investigate interaction effects of four operational process variables

	Inde	pendent Vari	ables	Dependent Variables	Constants		
pН	Т (°С)	Q (mL/min)	[ <i>H</i> 2 <i>O</i> 2] (ppm)	• Reaction time (t)			
4	20	1	0	<ul> <li>Final pH</li> <li>Apparent rate constant (k<sub>app</sub>)</li> </ul>	<ul> <li>Energy source (UV-LED)</li> <li>Initial BPA or DBP concentrations</li> </ul>		
10	40	10	2	<ul> <li>Degradation reaction efficiency (DRE)</li> </ul>	concentrations		

The output variables degradation reaction efficiency (DRE), assessed through reaction monitoring by NMR-1H, UV-Vis, and TOC.

**Note:** Variations in Reynolds numbers (all < 2500) were measured from the viscosity of the solutions at the set up and end of the reactions in a DV2T Brookfield viscometer.

### CONCLUSION

The experimental results of this study show that: 1) Increases in T and H2O2 increase DRE by ~40-70%; 2) Promoting laminar flow at Q=1 mL/min improves DRE by 2-10%; 3) Influence of pH value to reaction rate was better at the pH 10 values over pH 4; 4) The process yielded a 99.2 % /87.1% degradation efficiency of BPA/DBP with initial concentration of 100/10 mg L-1 at 15/120 min reaction time, respectively.

The use of a continuous-flow microreactor supported by TiO2 is a potential method for the treatment of wastewater contaminated by endocrine disruptors. Furthermore, this model could improve the DRE in a parallel array of microreactors, kind numbering up.

### FUTURE WORK / REFERENCES

#### Numbering up microreactors, enzymes inmovilization, and OLED's synthesis.

1. Singh, D.D. Epigenetic Mechanisms of Endocrine-Disrupting Chemicals in Breast Cancer and Their Impact on Dietary Intake. J. Xenobiot. 2025, 15, 1. https://doi.org/10.3390/jox15010001

2. Harkou, E.; Hafeez, S.; Manos, G.; Constantinou, A. CFD Study of the Numbering up of Membrane Microreactors for CO<sub>2</sub> Capture. Processes **2021**, *9*, 1515. https://doi.org/10.3390/pr9091515

3. Tonomura, O.; Taniguchi, S.; Nishi, K.; Nagaki, A.; Yoshida, J.-i.; Hirose, K.; Ishizuka, N.; Hasebe, S. Blockage Detection and Diagnosis of Externally Parallelized Monolithic Microreactors. Catalysts 2019, 9, 308. https://doi.org/10.3390/catal9040308

### ECCS2025.sciforum.net